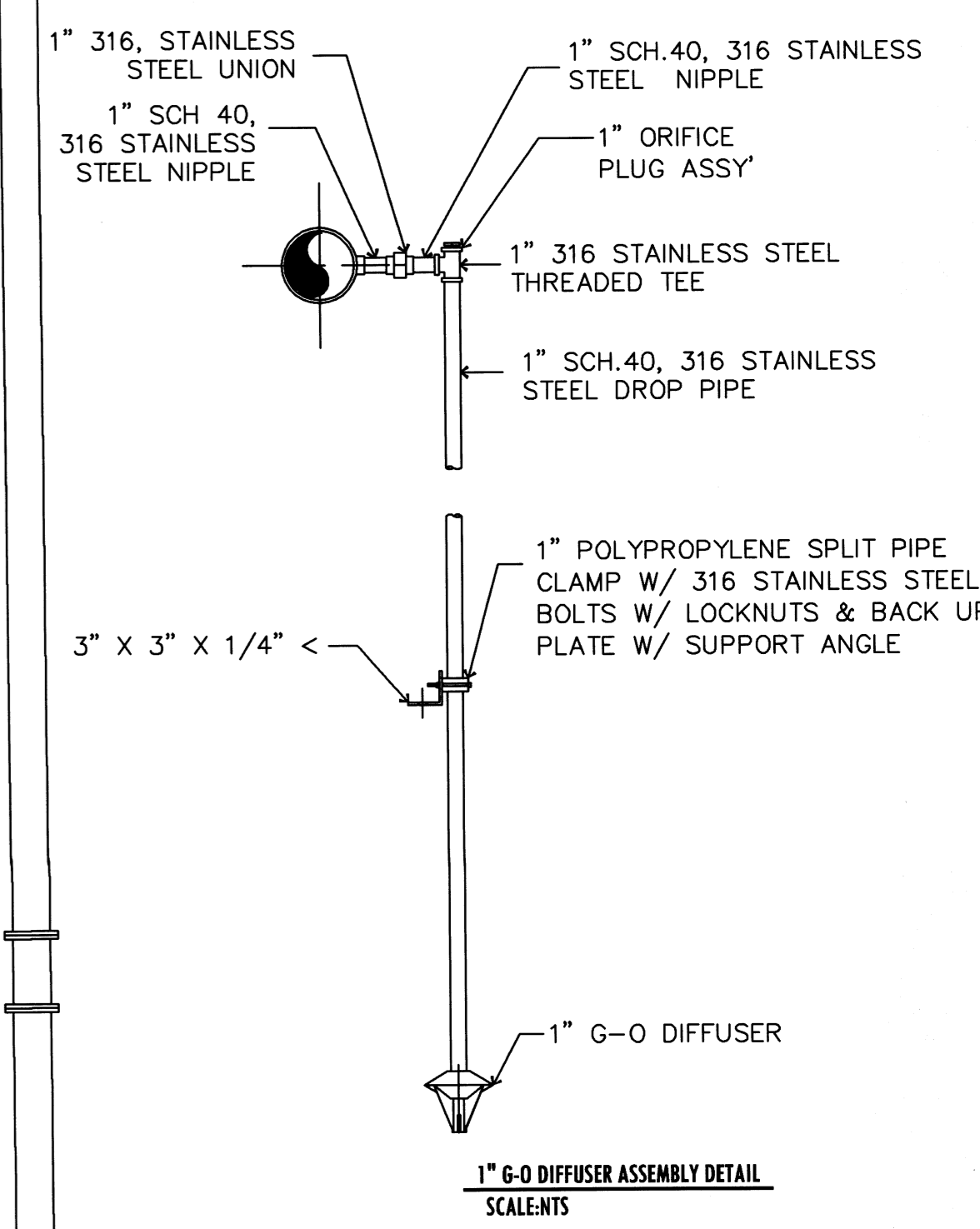
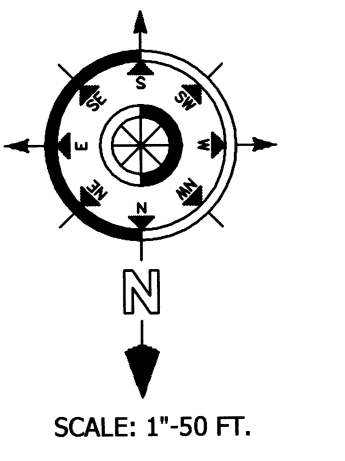


- NOTES**
1. REMOVE APPROXIMATELY 1,475 CY OF GRIT FROM EXISTING AERATION BASINS, INFLUENT CHANNEL, AND EFFLUENT CHANNEL. CONTRACTOR IS RESPONSIBLE FOR GRIT DISPOSAL.
 2. A SUFFICIENT AMOUNT OF GRIT MUST BE REMOVED TO RESTORE ALL FAILED AERATION ASSEMBLIES.
- ▲ ADDENDUM No.1: REVISED AIR SUPPLY MODIFICATIONS TO INCLUDE THERMAL MASS FLOWMETER, SPECIFIED SCHEDULE 40 FOR ALL AIR SUPPLY LINES.



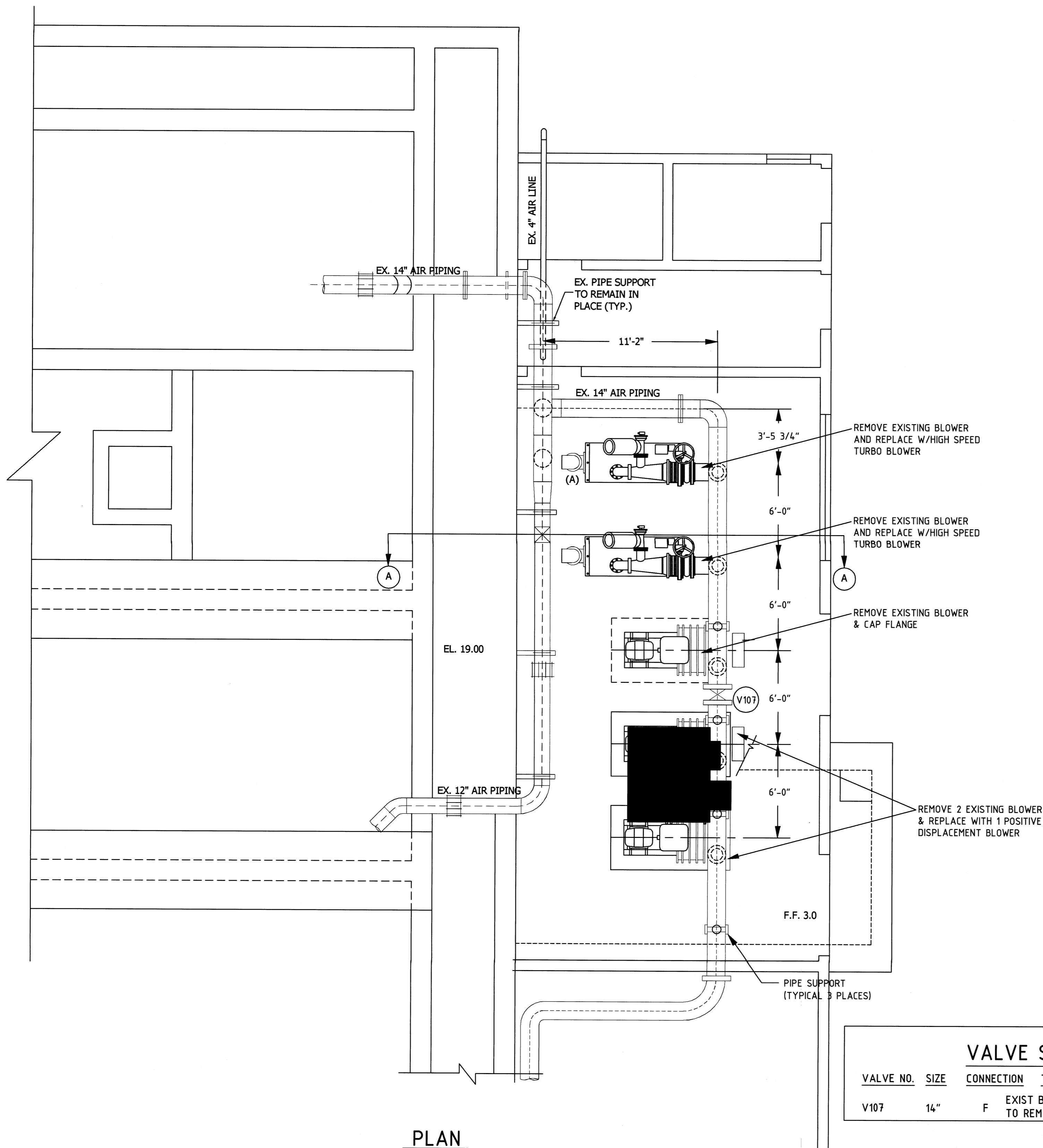
NOTE: Remove grit from existing basins as required to restore all 1\"/>

Seal

Laguna Madre Water District
Wastewater Treatment Plants Rehabilitation
 September 2016

Isla Blanca WWTP
Site Plan And
Mechanical Modifications
To Existing Plant

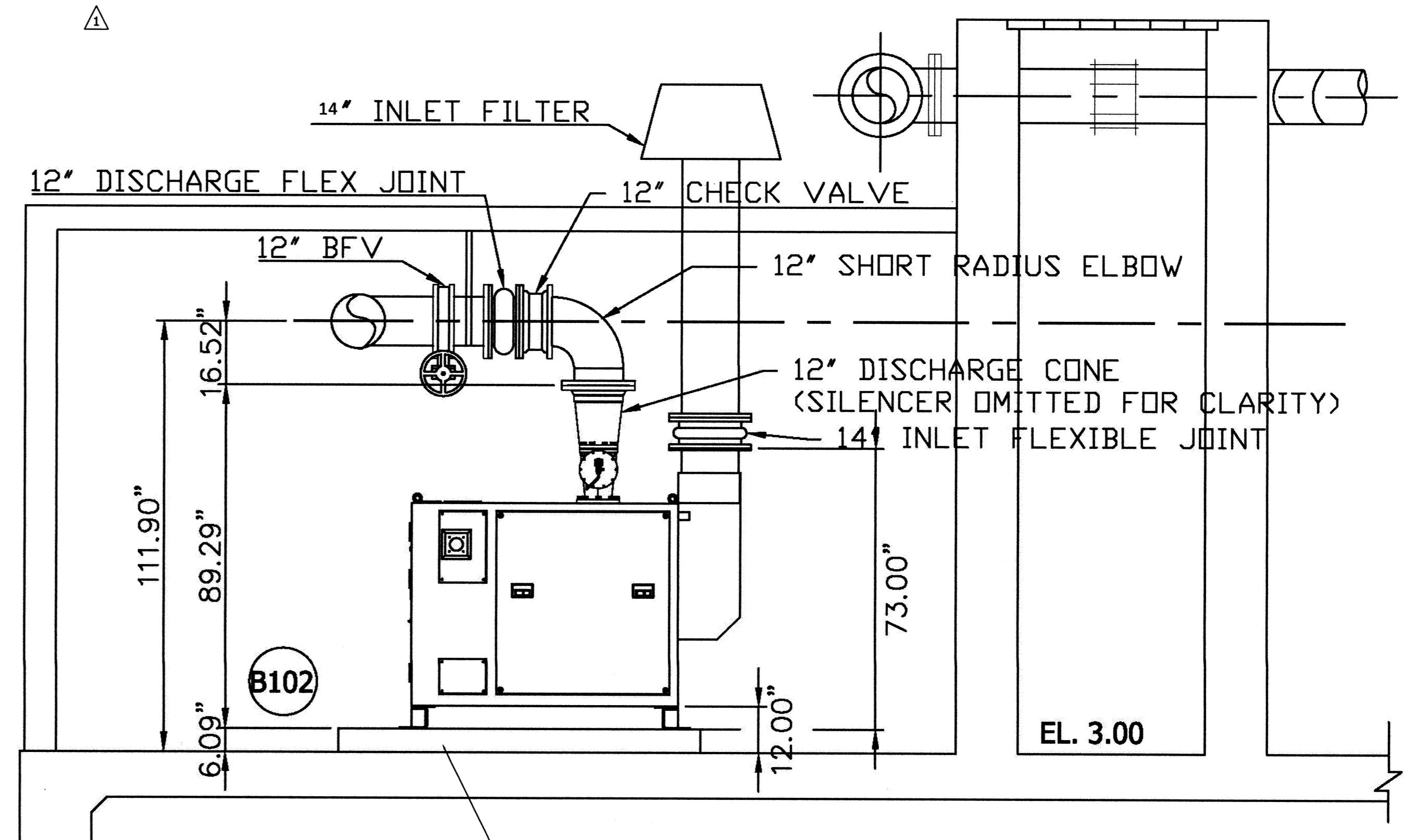
4



PLAN
SCALENTS

VALVE SCHEDULE

VALVE NO.	SIZE	CONNECTION	TYPE	COMMENTS
V107	14"	F	EXIST BUTTERFLY VALVE TO REMAIN IN PLACE	HANDWHEEL OPERATOR



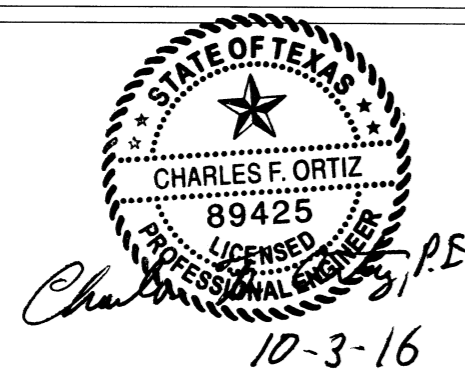
PROFILE, SECTION A-A

NOTE: LAYOUT IS PRELIMINARY. FINAL LAYOUT TO BE PROVIDED IN SUBMITTALS.

GENERAL NOTES

EACH BLOWER SHALL BE PROVIDED WITH A VERTICALLY MOUNTED INTAKE FLANGE AND A CARTRIDGE TYPE INTAKE FILTER SILENCER TO REDUCE ENTRANCE OF RAIN WATER, MOISTURE, AND DUST INTO THE BLOWER INLET. FILTER SILENCER SHALL BE CARTRIDGE-TYPE WITH WEATHER HOOD AND WITH 125# ANSI FLANGED OUTLET SIZED TO FIT THE BLOWER INLET PIPING WITHOUT REQUIREMENT FOR REDUCERS OR TRANSITIONS. FILTER SILENCER SHALL BE POWDER COATED AND SUITABLE FOR CONTINUOUS WEATHER EXPOSURE IN EXTERIOR LOCATIONS. FILTER SILENCER SHALL BE ENDUSTRA "TRI-VENT SERIES P09" WITH ELEMENT E047937P WITH 98% EFFICIENT @ 10-MICRON (NOMINAL) HYDROPHOBIC MEDIUM ADHESIVE POTTED ON ALL FOUR SIDES WITHIN A GALVANIZED STEEL FRAME WITH FULL FACE GASKET ON DOWNSTREAM SIDE, AND SHALL FIT TIGHTLY WITHIN THE FILTER FRAME TO DISCOURAGE AIR BYPASS.

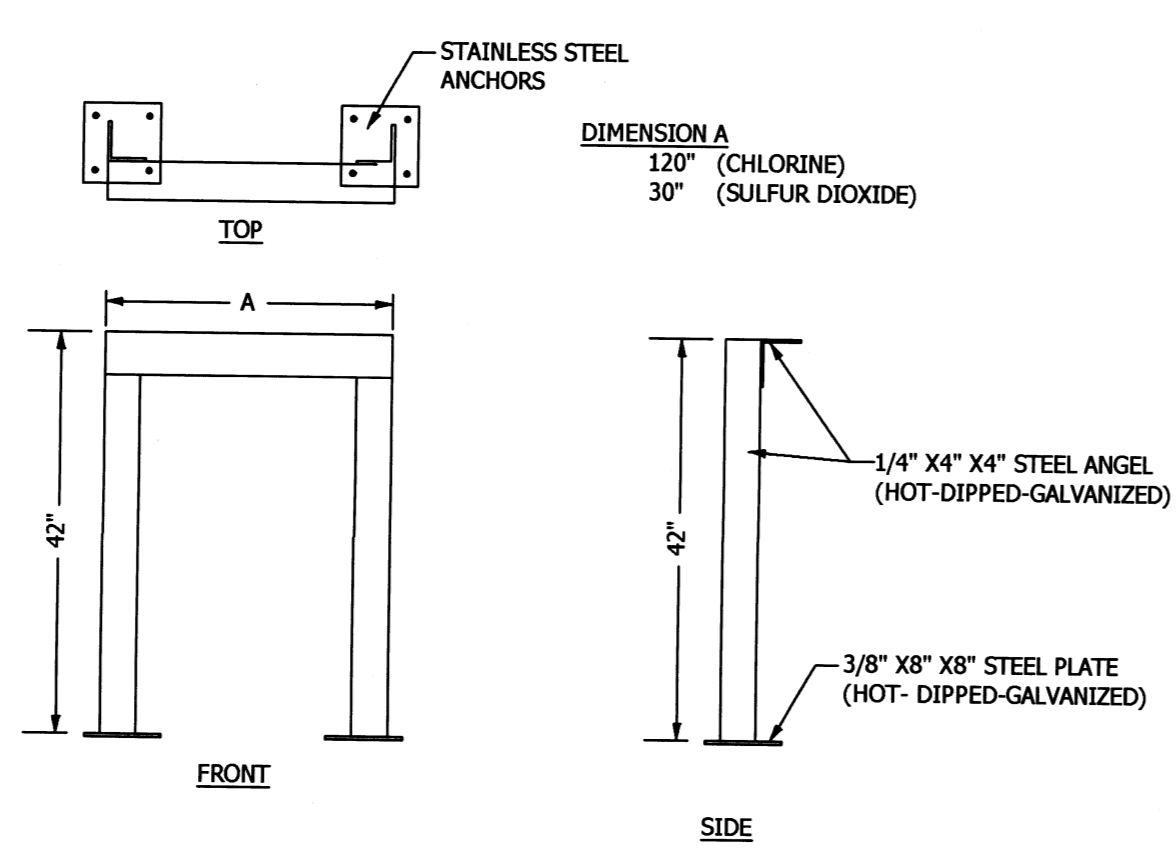
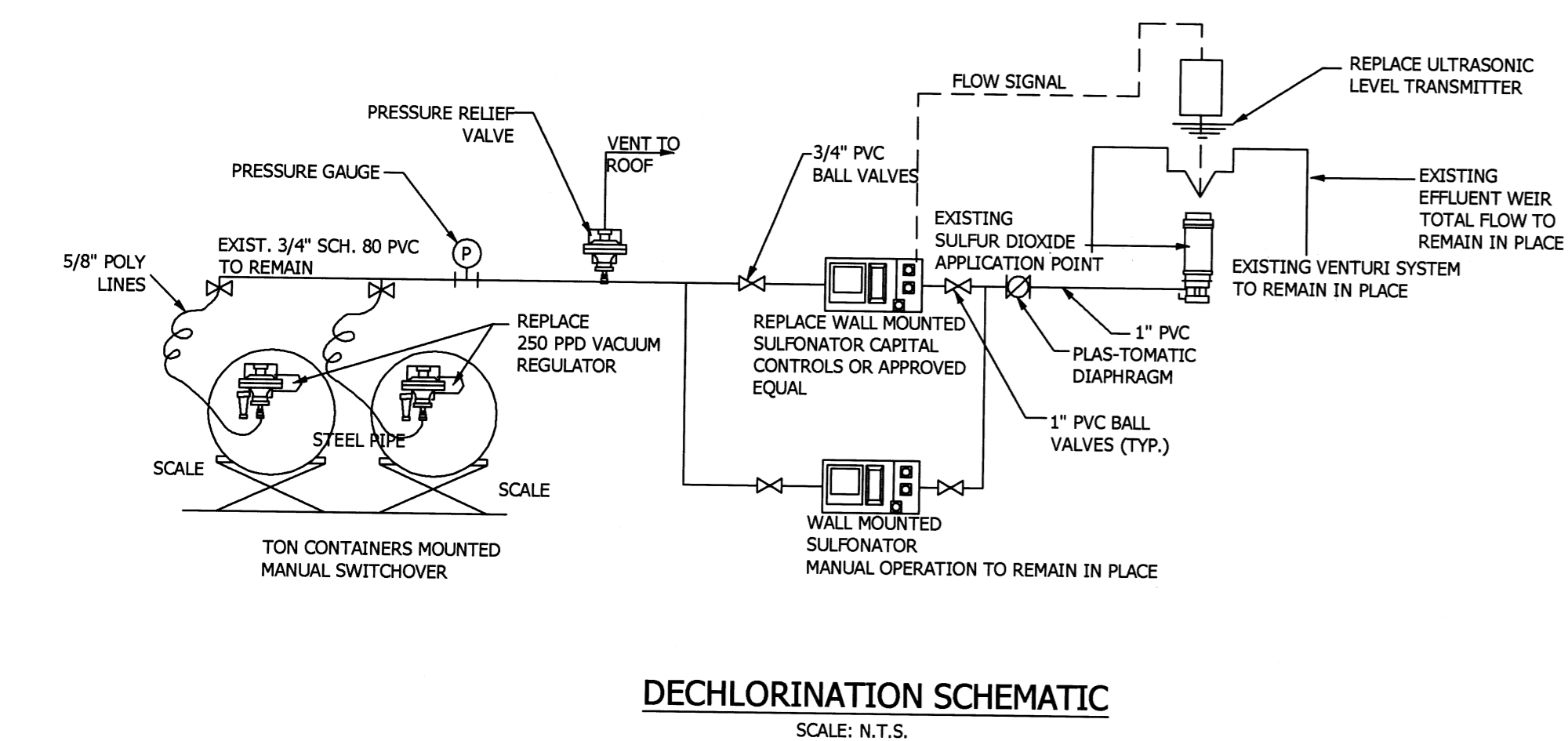
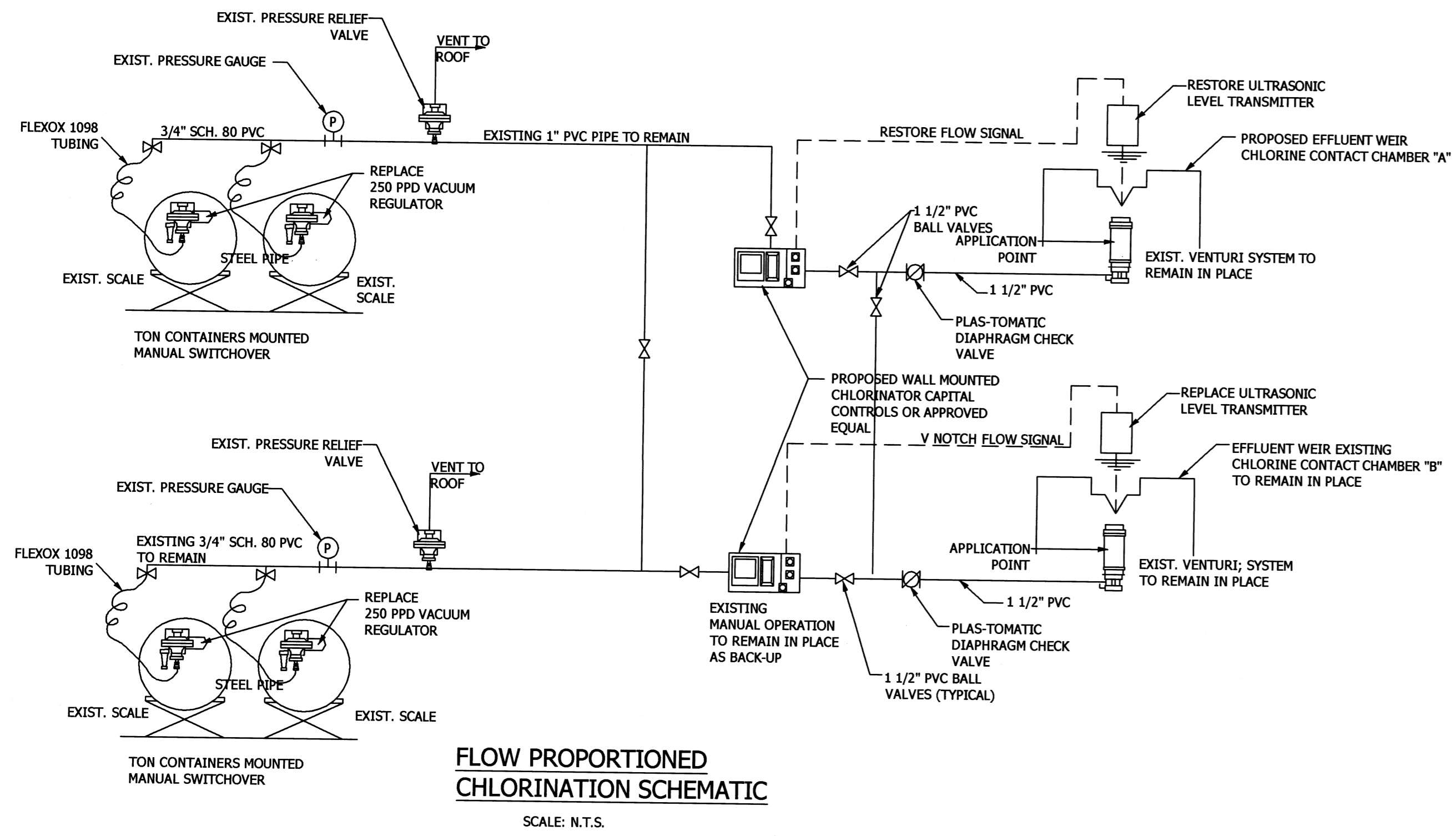
NOTES:
ADDENDUM No1: REVISED TURBO BLOWER PROFILE VIEW FOR BASE BID. BLOWERS MUST BE ELEVATED 12-INCHES ABOVE FINISHED FLOOR ELEVATION TO STAY ABOVE THE 100-YR FLOOR PLAIN.



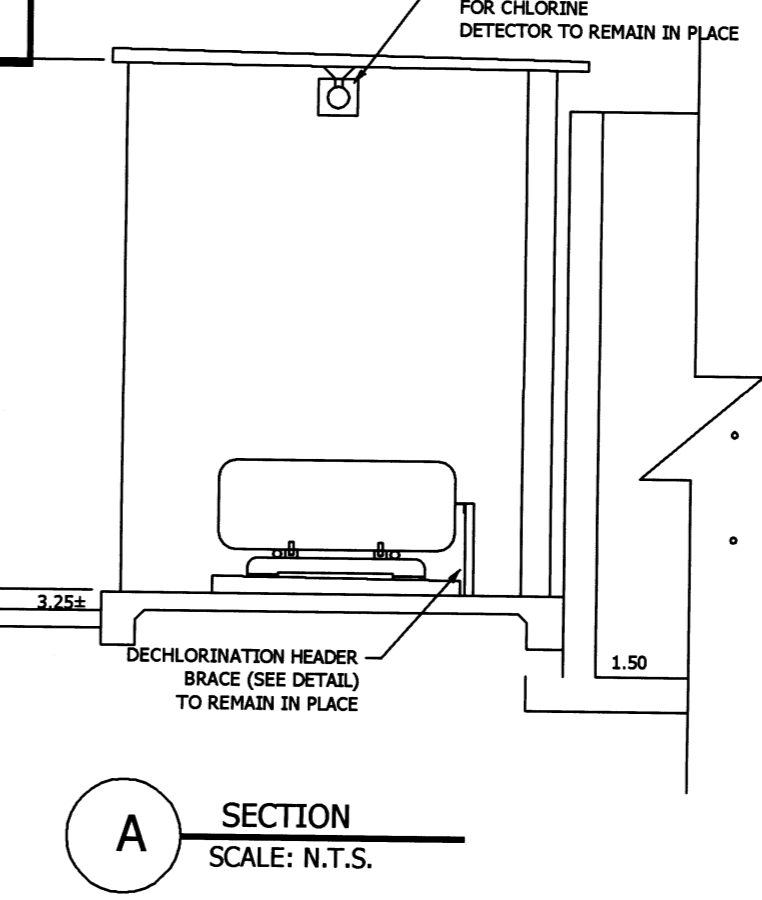
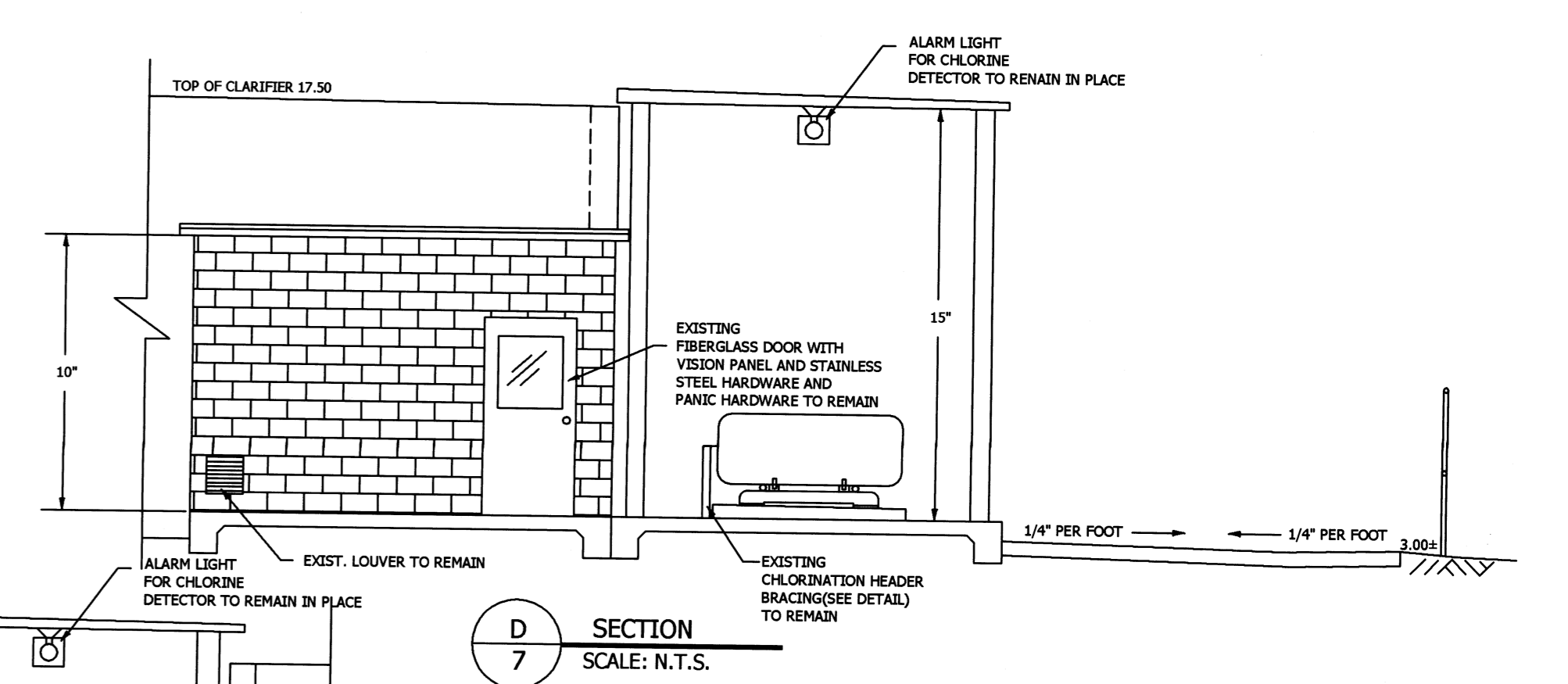
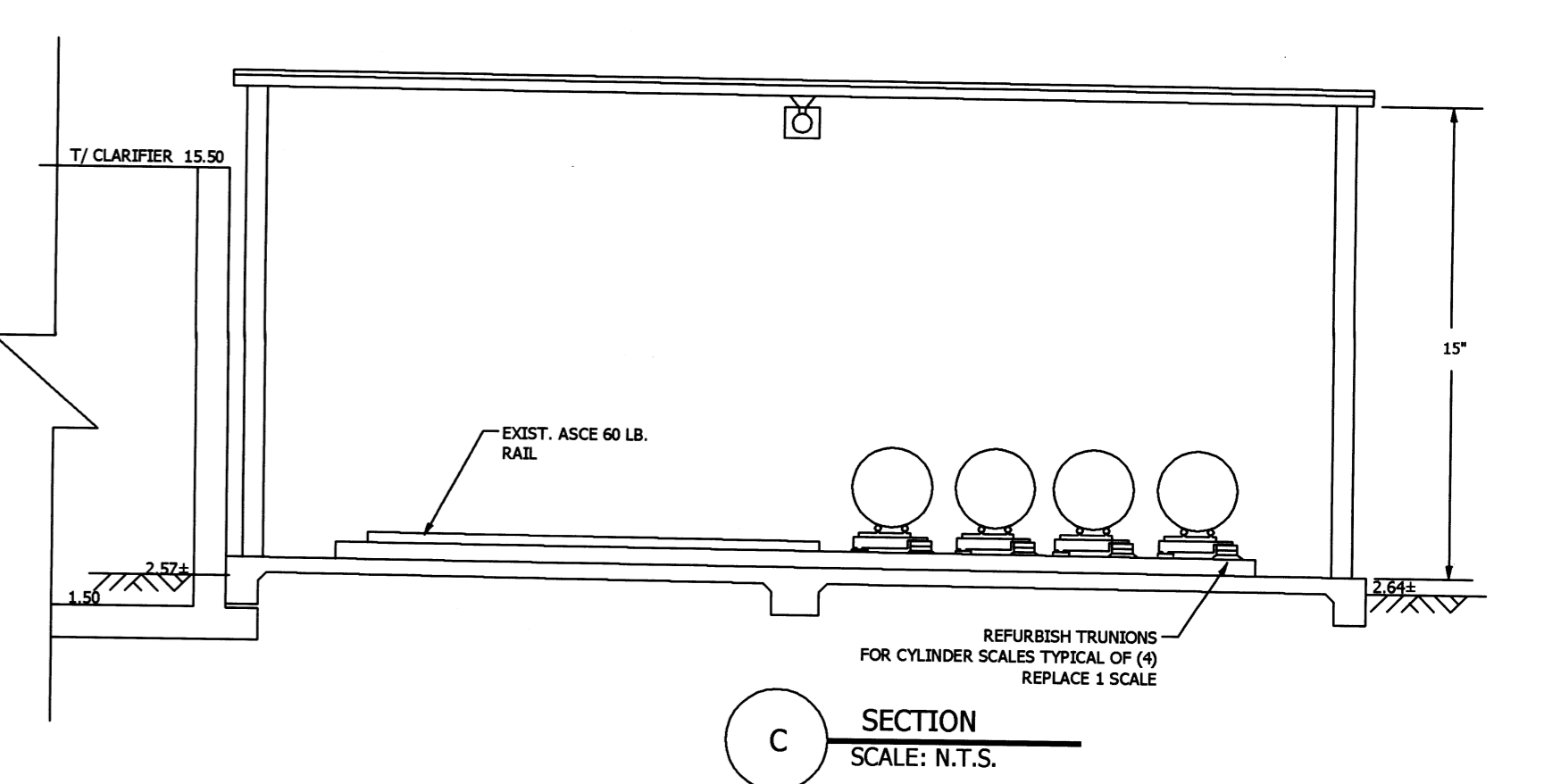
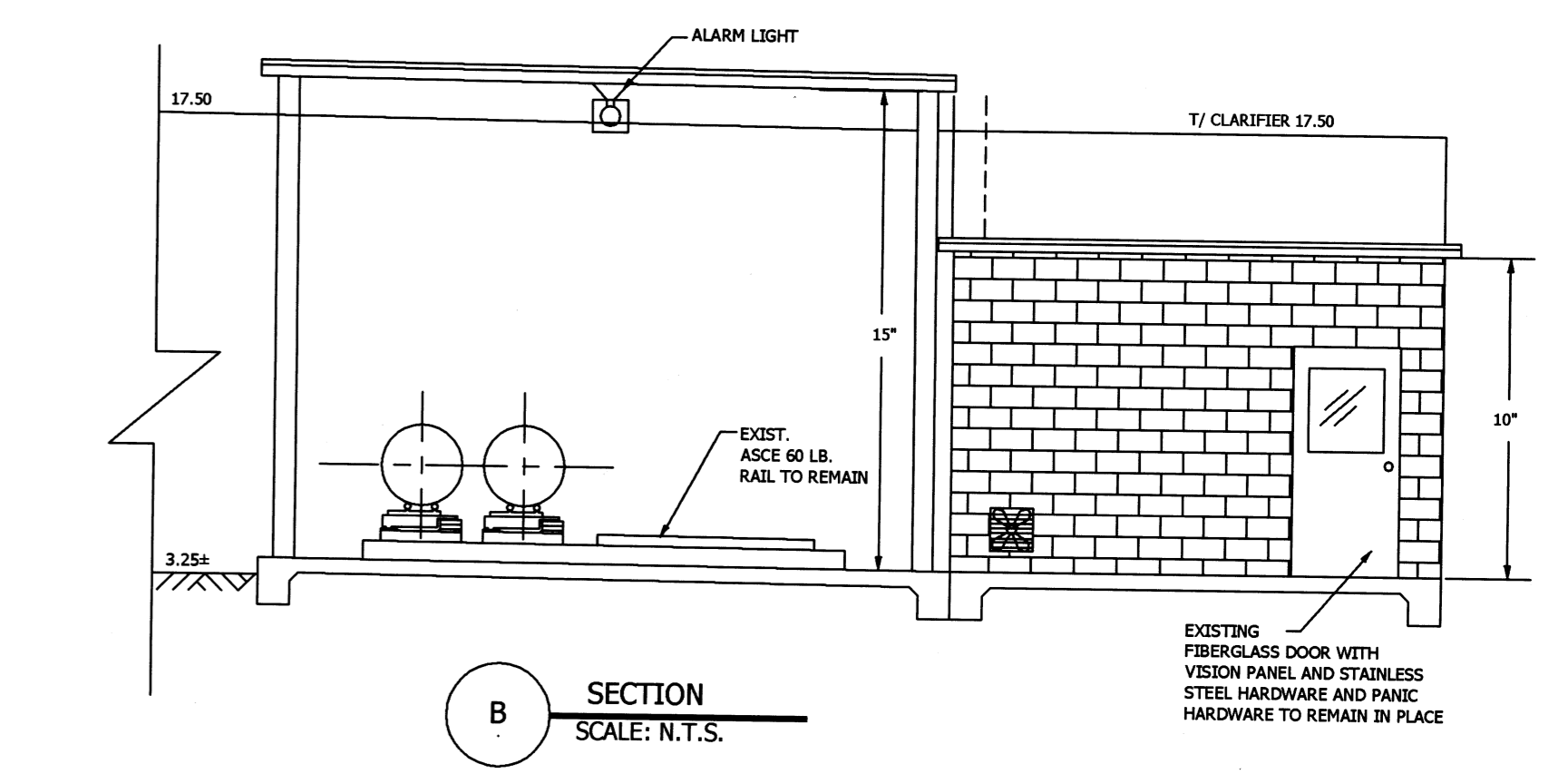
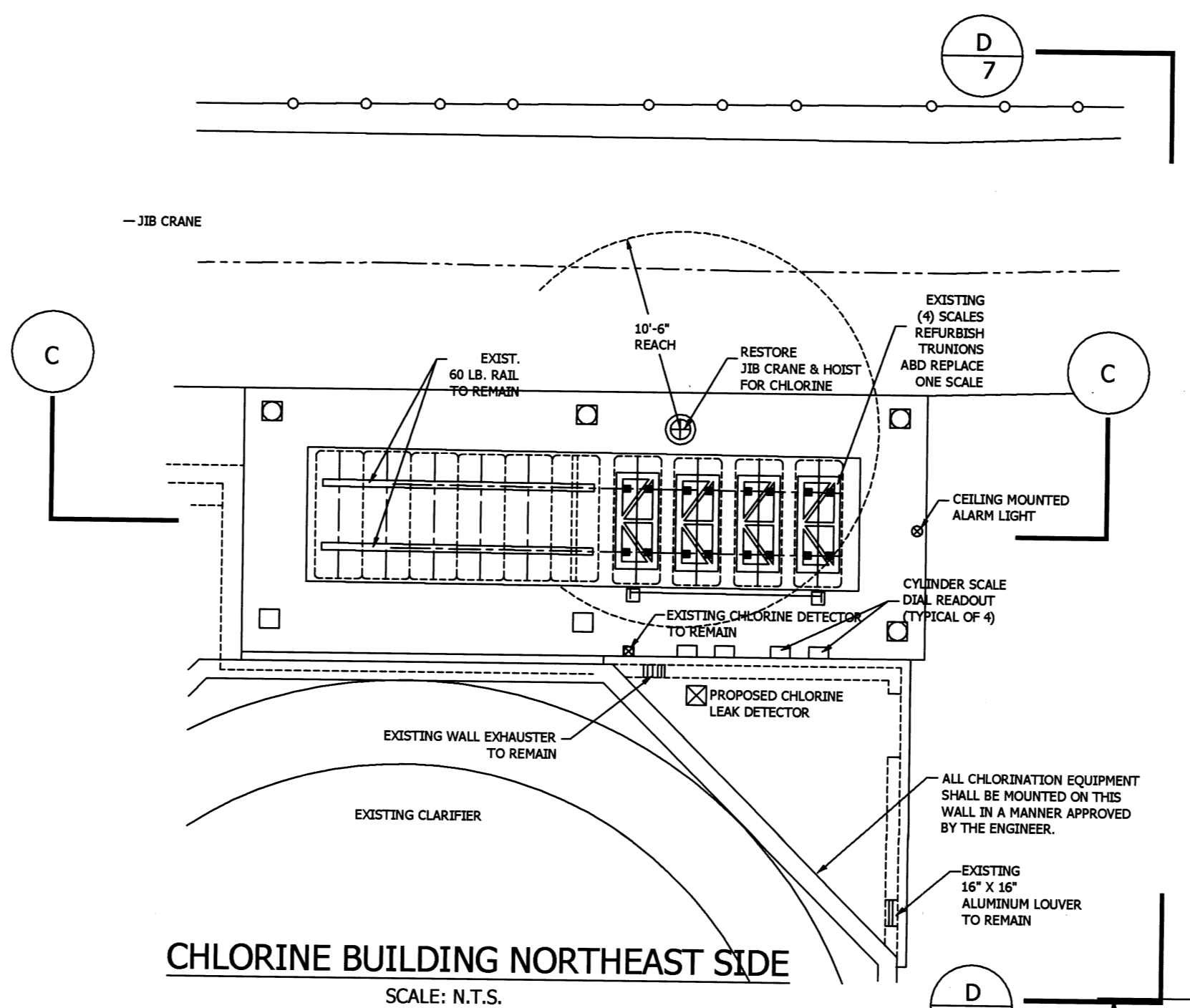
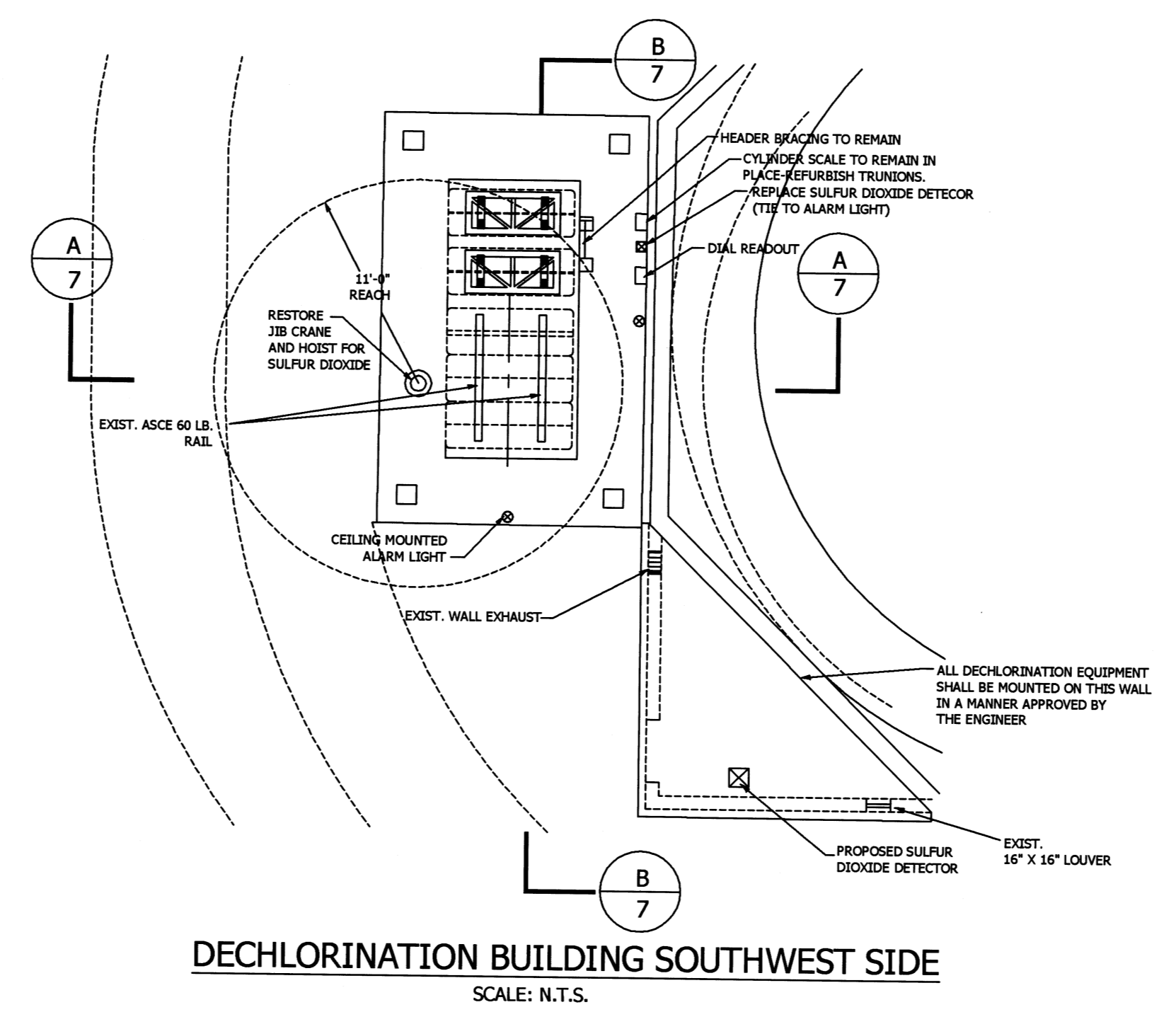
Laguna Madre Water District
Wastewater Treatment Plants Rehabilitation
September 2016

Isla Blanca WWTP
Blower Modifications

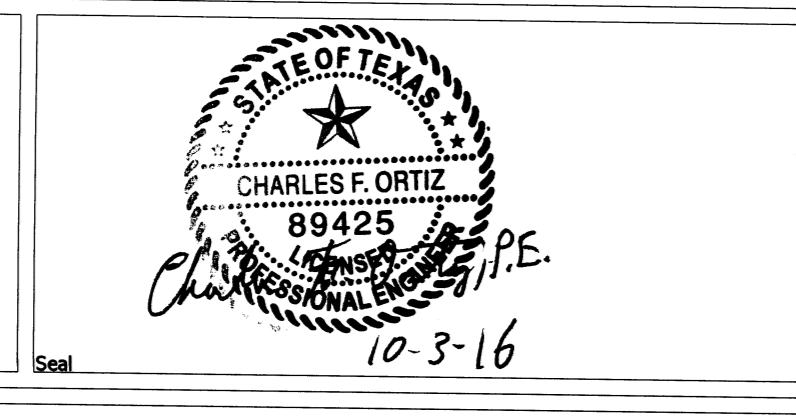




- CHLORINE AND SULFUR DIOXIDE HOISTS**
- 1) FOR JIB CRANES, REPLACE CORRODED ROLLERS, AND HARDWARE (NUTS & BOLTS), AND BEARINGS; INSTALL A ROTATION STOP.
 - 2) REPLACE EXISTING HOIST AND TROLLEY SEE SECTION 467400 - HOIST IN SPECIFICATIONS, EXISTING POWER IS IN GOOD CONDITION AND CAN REMAIN IN PLACE.



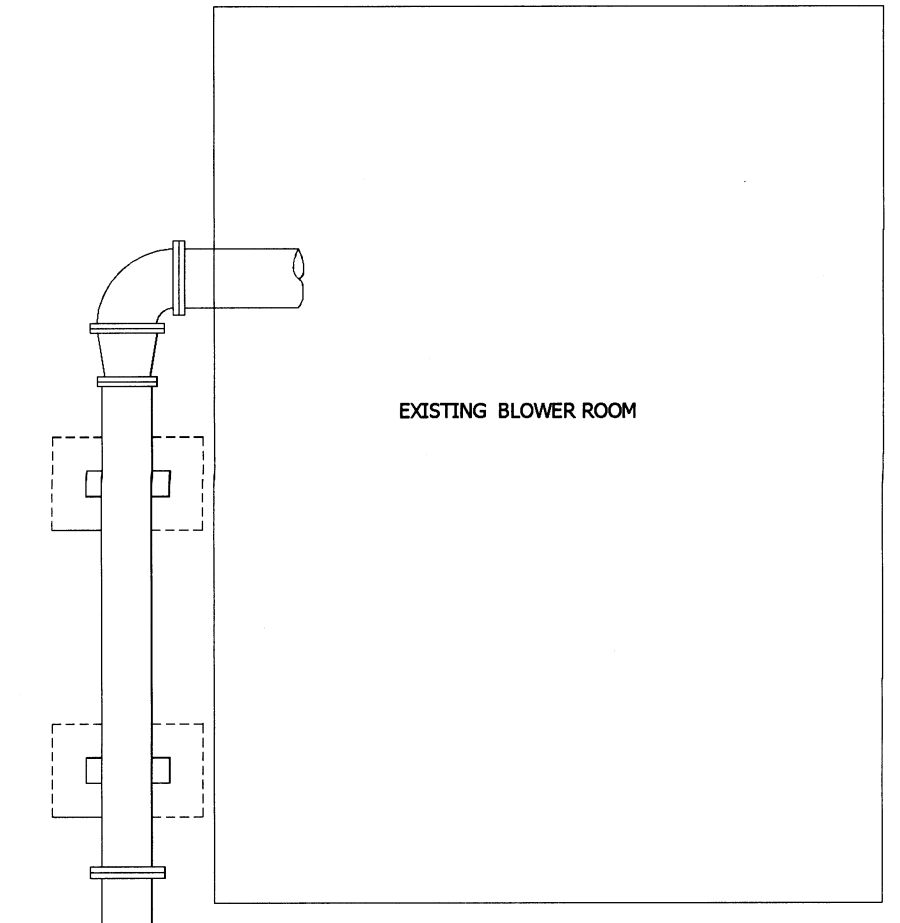
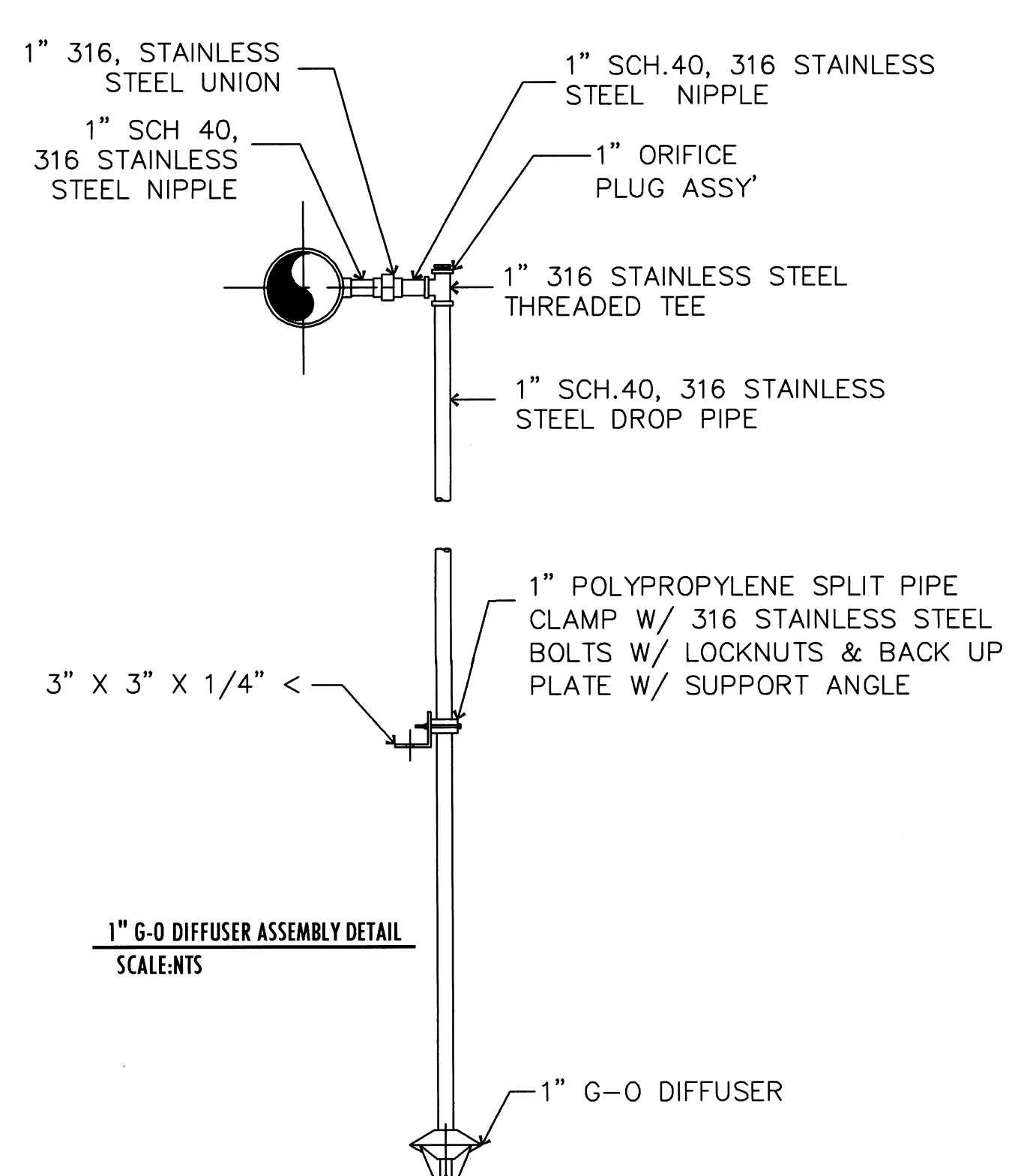
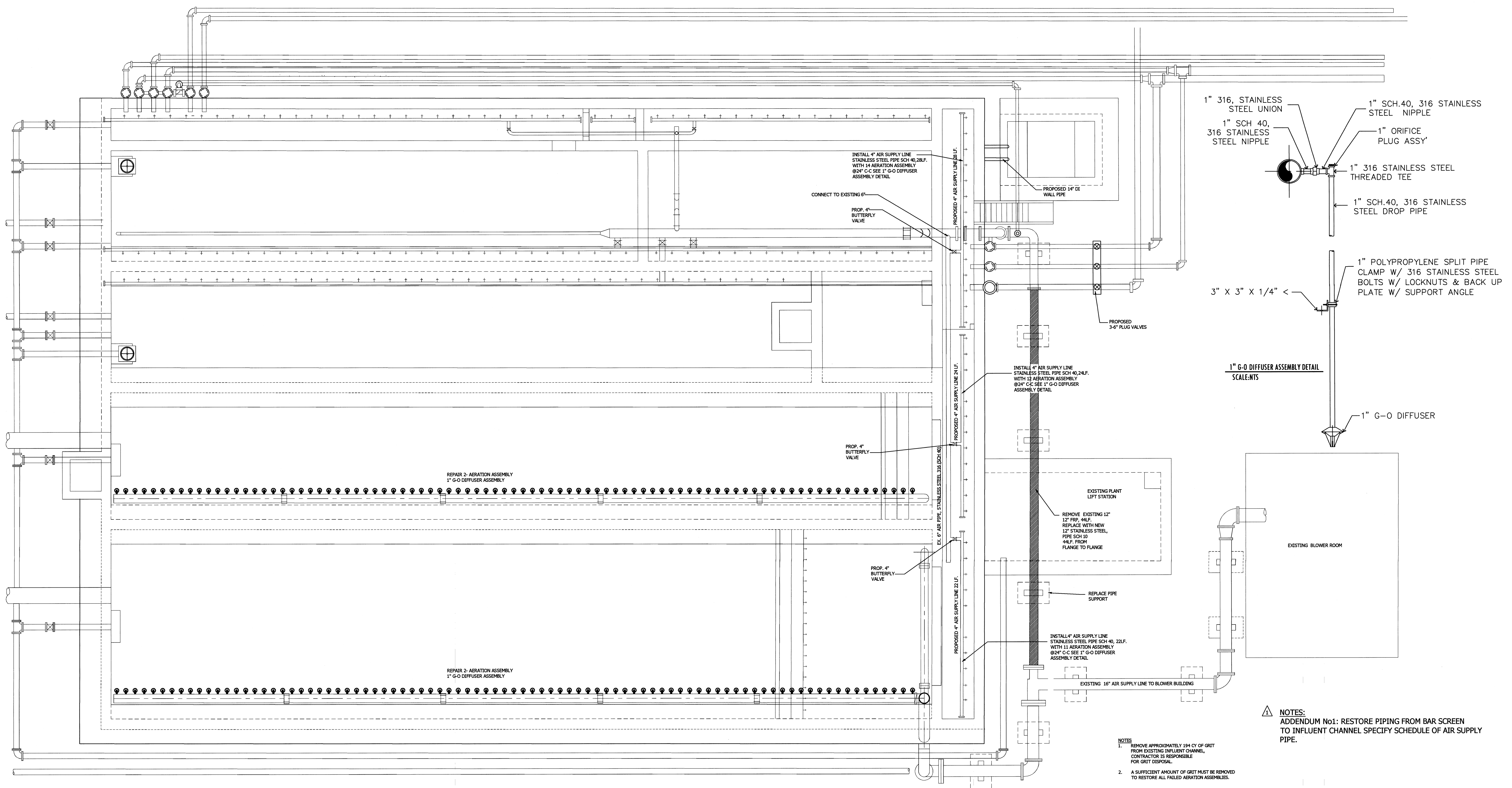
NOTES:
ADDENDUM No1: SIZE ALL PROPOSED ROTAMETERS FOR 250 PPD. DISTRICT DOES NOT USE INDUCTION PUMPS FOR CHLORINATION AND DECLORINATION EQUIPMENT. EXISTING VENTURI SYSTEM TO REMAIN IN PLACE. AUTOMATIC SWITCHOVER REMOVED FROM ALL VACUUM REGULATORS. RESTORE EJECTORS AT ALL SITES.



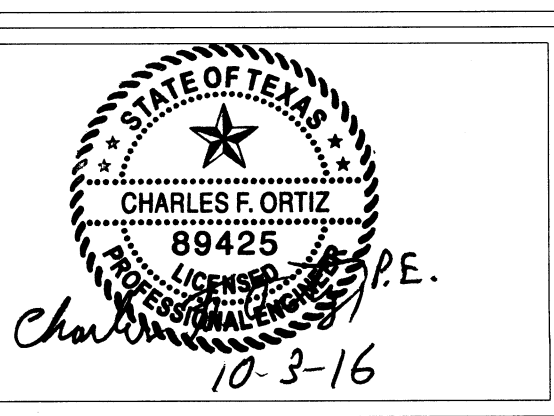
Laguna Madre Water District
Wastewater Treatment Plants Rehabilitation
September 2016

Isla Blanca WWTP
Chlorination & Dechlorination
Equipment





- NOTES:**
- ADDENDUM No1: RESTORE PIPING FROM BAR SCREEN TO INFLUENT CHANNEL SPECIFY SCHEDULE OF AIR SUPPLY PIPE.
1. REMOVE APPROXIMATELY 194 CY OF GRIT FROM EXISTING INFLUENT CHANNEL. CONTRACTOR IS RESPONSIBLE FOR GRIT DISPOSAL.
2. A SUFFICIENT AMOUNT OF GRIT MUST BE REMOVED TO RESTORE ALL FAILED AERATION ASSEMBLIES.



Laguna Madre Water District
 Wastewater Treatment Plants Rehabilitation
 September 2016

Laguna Madre Water District
 Andy Bowie Wastewater Plant
 Site Plan and Mechanical Modifications To
 Air Supply Line

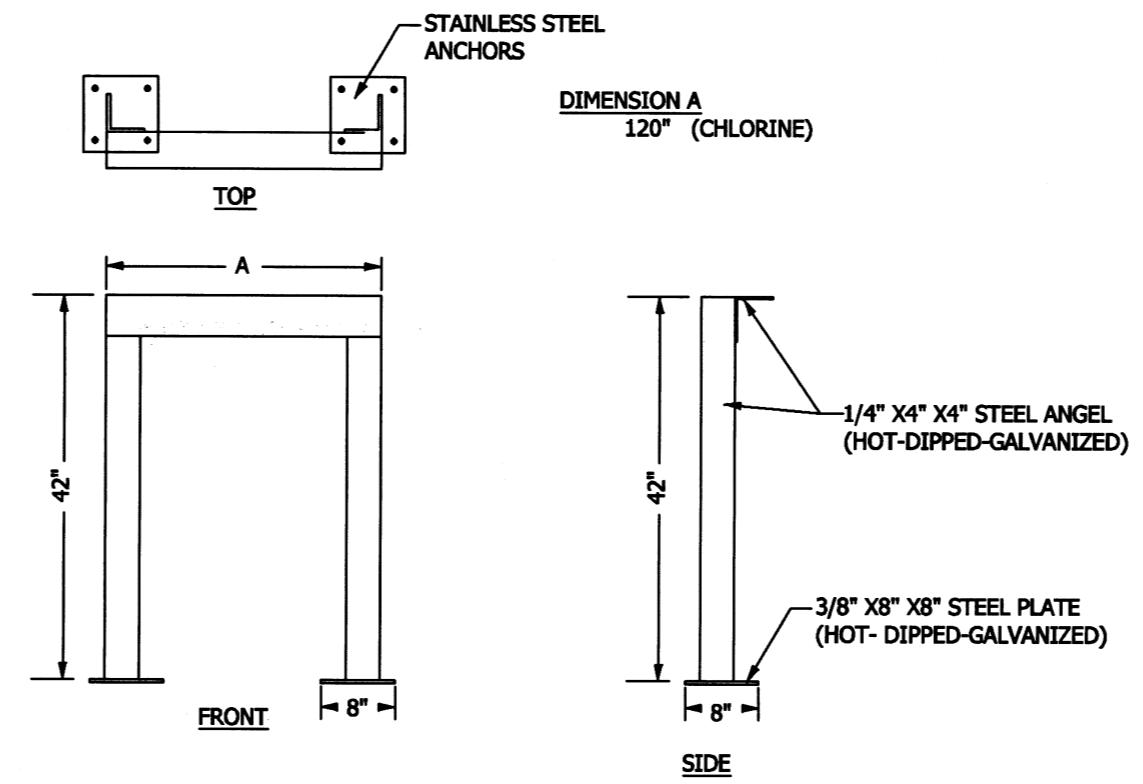


GENERAL NOTES

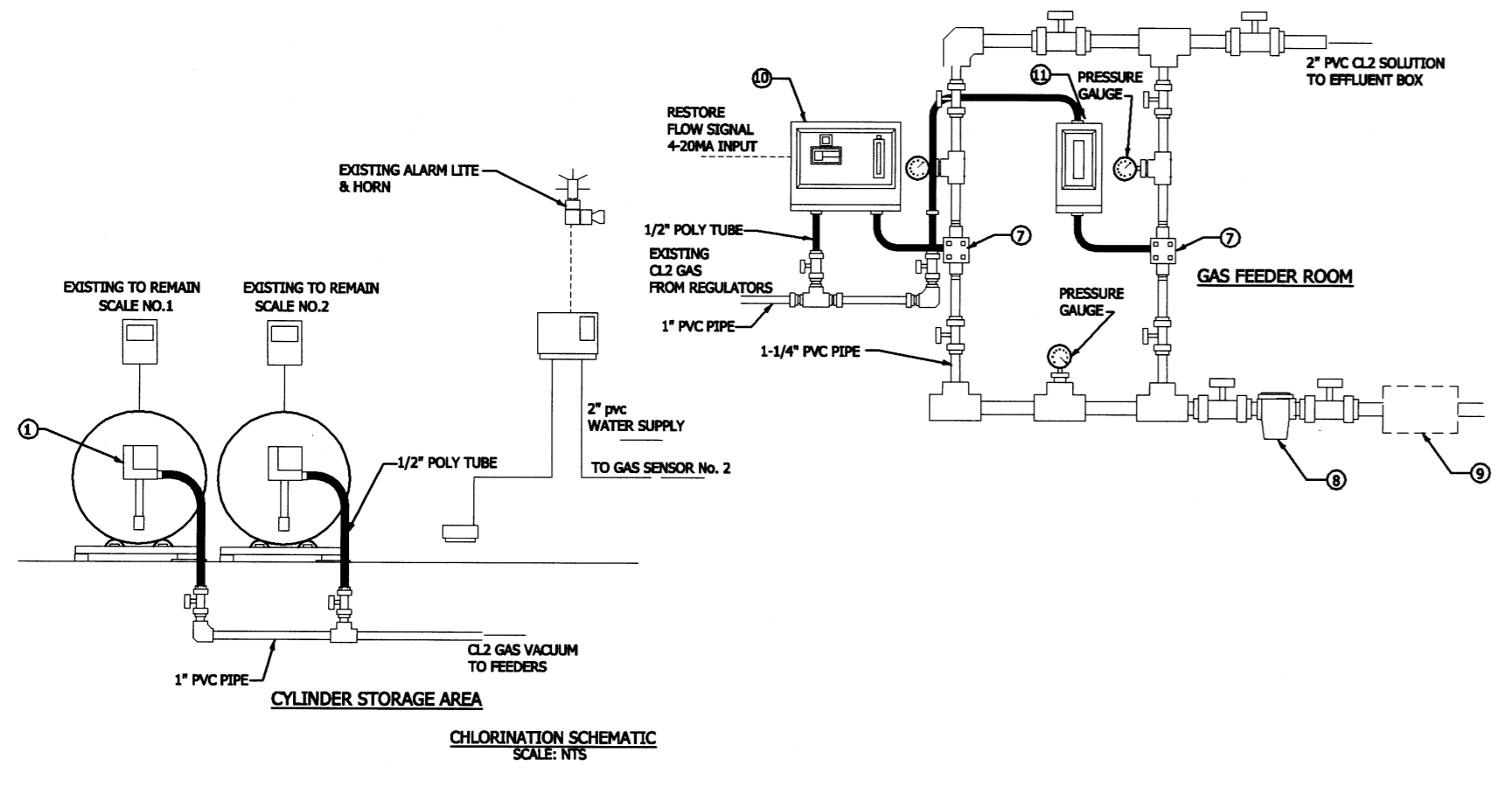
THE SULFUR DIOXIDE AND CHLORINE SCHEMATIC IS PROVIDED FOR GUIDANCE. THE CONTRACTOR IS RESPONSIBLE FOR PROVIDING A DETAILED SUBMITTAL LAYOUT SHOWING PIPING, FITTINGS, VALVES, SIZES, ELEVATIONS, ETC. OF THE SYSTEM TO PROVIDE AN OPERATIONAL SYSTEM. THE SULFUR DIOXIDE AND CHLORINE SYSTEM INSIDE THE FIBERGLASS ENCLOSURE SHALL BE WALL MOUNTED. THE CONTRACTOR IS REQUIRED TO MAINTAIN THE GUIDELINES OF THE SCHEMATIC AND INCLUDE ANY ADDITIONAL FITTINGS OR VALVES NOT SHOWN IN THE SCHEMATIC TO PROVIDE AN OPERATIONAL SYSTEM.

ALL NECESSARY CHEMICAL FEED PLANT SHUT-DOWNS WILL BE COORDINATED WITH THE OPERATOR.

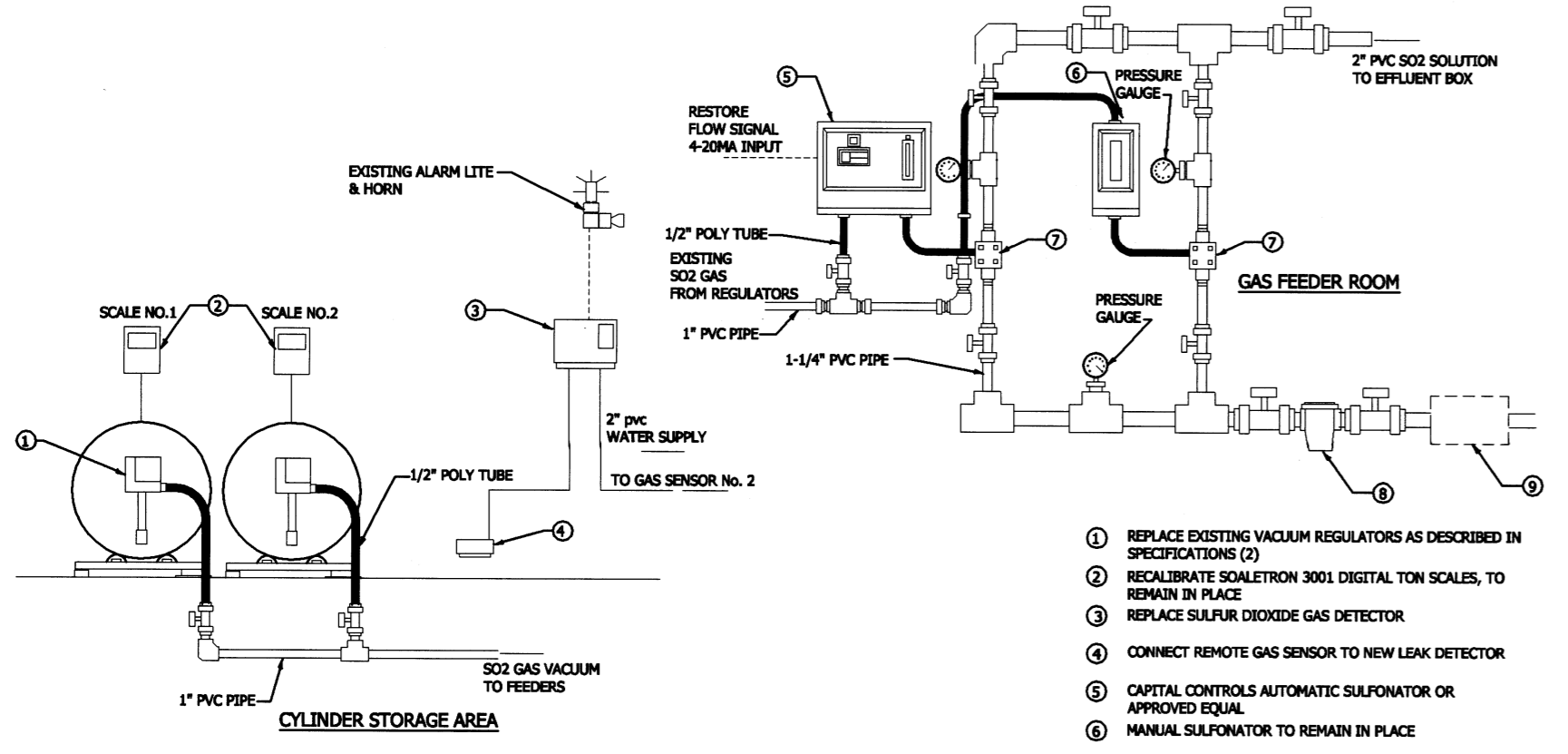
ALL PIPE SUPPORTS AND BRACING FOR ALL CHEMICAL FEED SYSTEMS (SULFUR DIOXIDE AND CHLORINE) SHALL BE STAINLESS STEEL WITH STAINLESS STEEL ANCHORS.



EXISTING CHLORINATION/DECHLORINATION HEADER BRACING TO REMAIN



CHLORINATION SCHEMATIC SCALE: NTS



DECHLORINATION SCHEMATIC SCALE: NTS

1. REPLACE EXISTING VACUUM REGULATORS AS DESCRIBED IN SPECIFICATIONS (2)
2. RECALIBRATE SCALES FROM 3000 DIGITAL TON SCALES, TO REMAIN IN PLACE
3. REPLACE SULFUR DIOXIDE GAS DETECTOR
4. CONNECT REMOTE GAS SENSOR TO NEW LEAK DETECTOR
5. CAPITAL CONTROLS AUTOMATIC SULFONATOR OR APPROVED EQUAL
6. MANUAL SULFONATOR TO REMAIN IN PLACE
7. REPLACE EXISTING 1-1/4" EXTRACTOR ASSEMBLY
8. EXISTING 2" PVC BASKET STRAINER TO REMAIN IN PLACE
9. EXISTING BACKFLOW PREVENTER TO REMAIN IN PLACE
10. CAPITAL CONTROLS AUTOMATIC CHLORINATION OR APPROVED EQUAL
11. MANUAL CHLORINATOR TO REMAIN IN PLACE

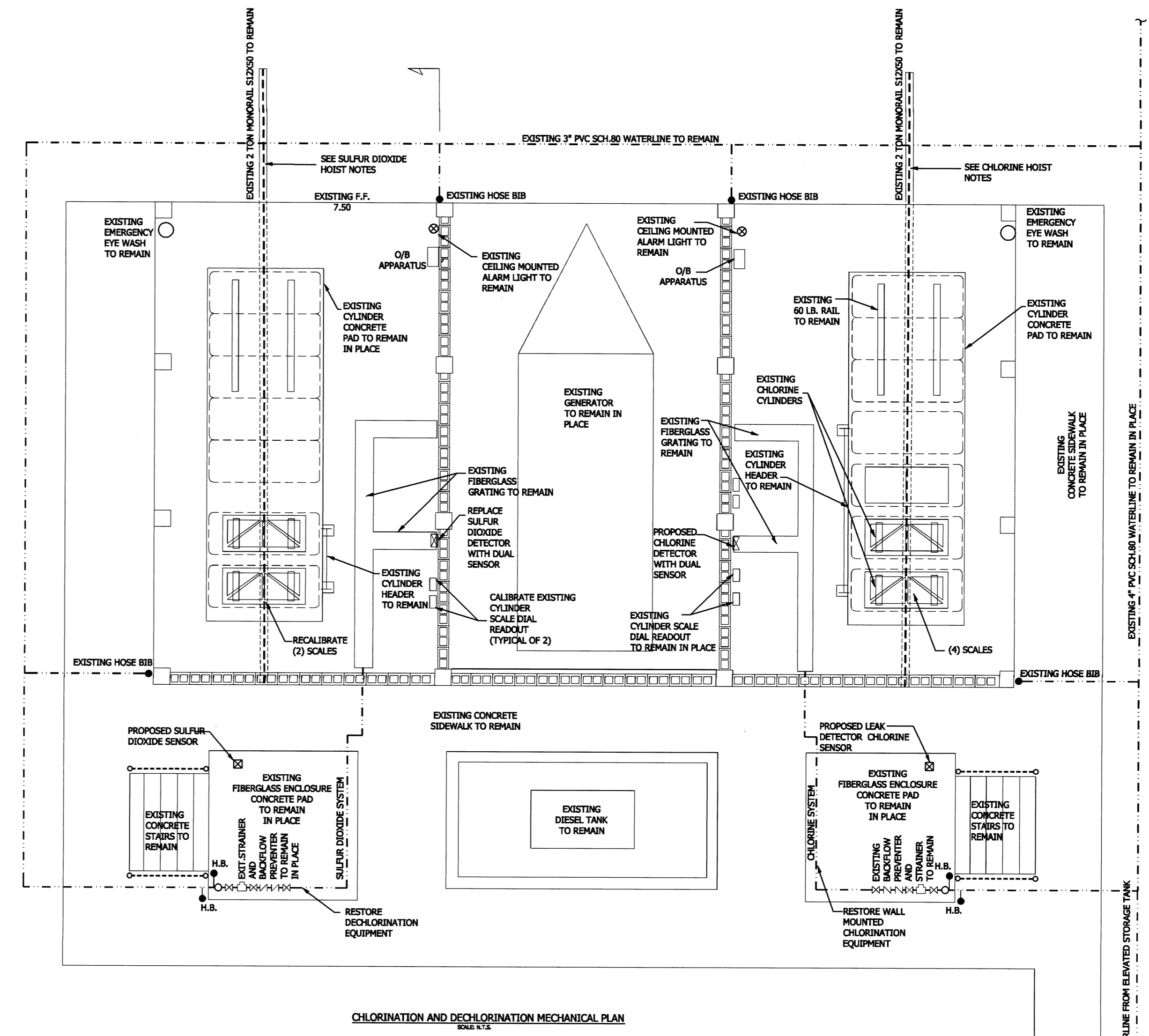
CHLORINE HOIST NOTES

1. MONORAIL (EXISTING S12X50 BEAM TO REMAIN)
 - A. REPLACE NUTS & BOLTS TO COMPLY WITH ANSI B30.11-L3 2(B). USE BEVELED WASHERS.
2. REPLACE TROLLEY AND HOIST. SEE SECTION 46 7400-HOIST IN SPECIFICATIONS.
 - A. EXISTING ELECTRIFICATION / POWER IS IN GOOD CONDITION.

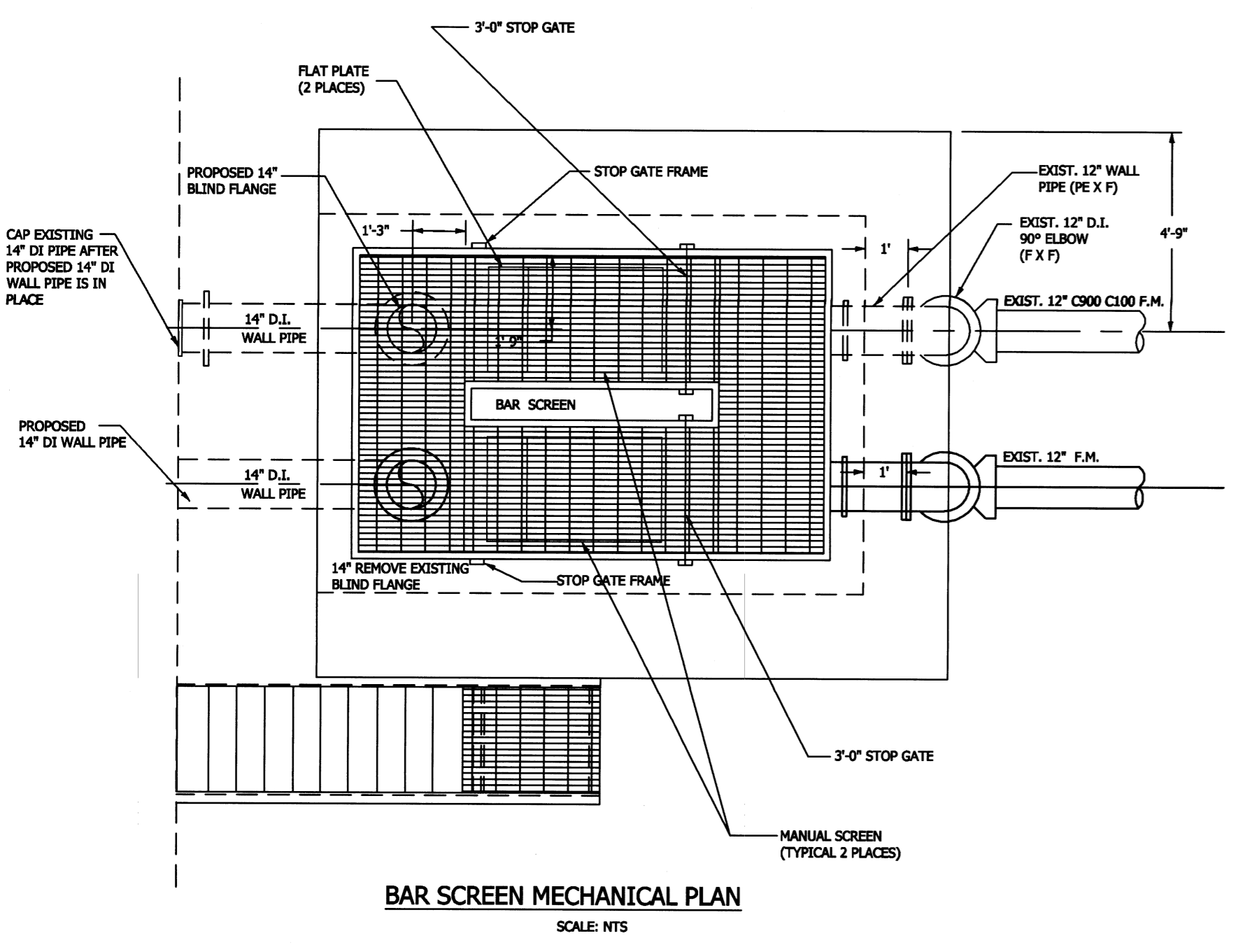
SULFUR DIOXIDE HOIST NOTES

1. MONORAIL (EXISTING S12X50 BEAM TO REMAIN)
 - A. REPLACE NUTS & BOLTS TO COMPLY WITH ANSI-B 30.11-3.2(B) USE BEVELED WASHERS.
 - B. REPLACE FESTOON HARDWARE AND WIRE. INSTALL DISCONNECT THAT IS READILY ACCESSIBLE TO PROVIDE A MEANS TO OPEN THE POWER CIRCUIT.
2. REPLACE TROLLEY AND HOIST. SEE SECTION 467400-HOIST IN SPECIFICATIONS.
 - A. EXISTING ELECTRIFICATION / POWER IS IN GOOD CONDITION.

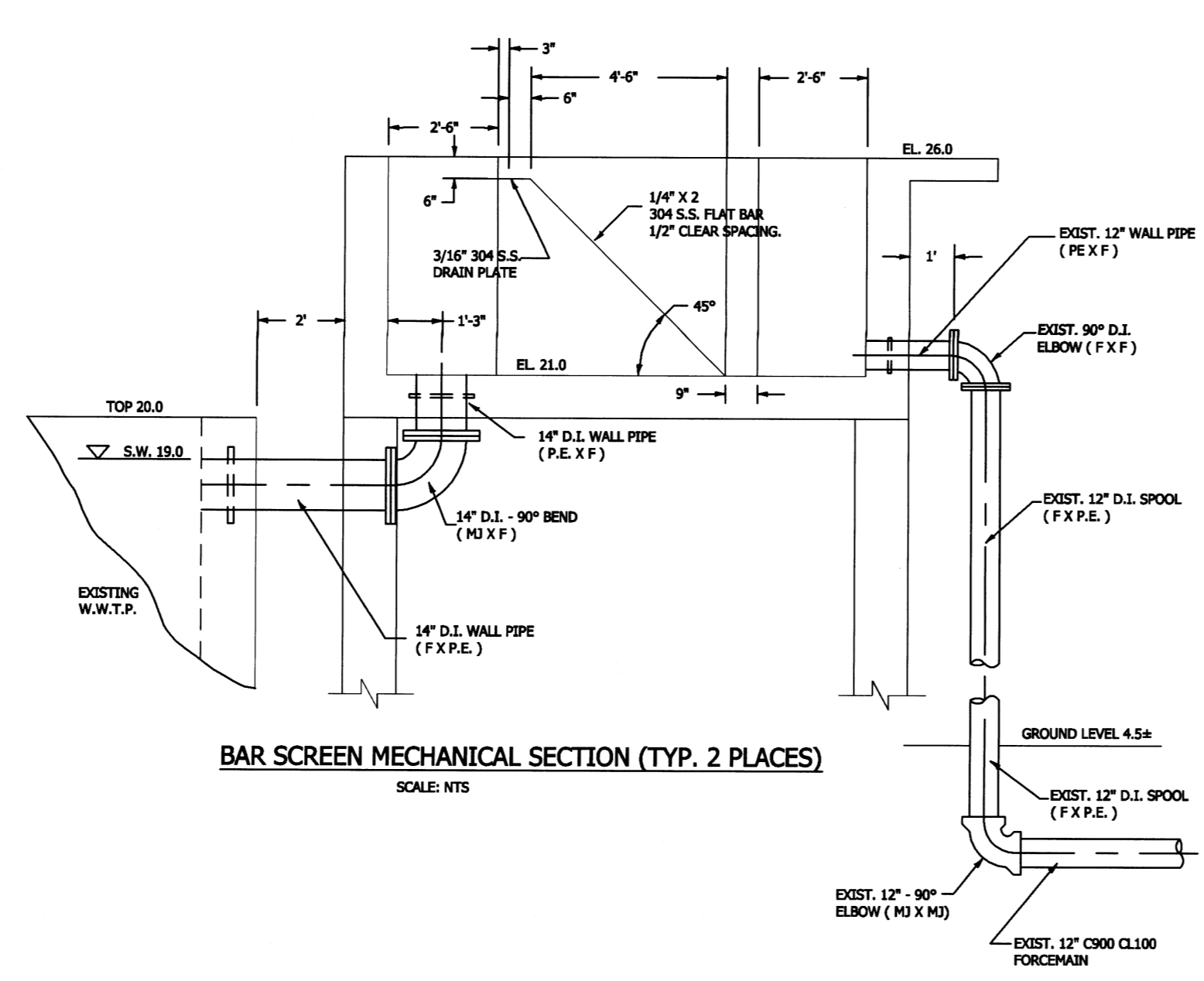
NOTES:
 ADDENDUM No.1: PROVIDE DUAL SENSOR FOR CHLORINE AND SULFUR DIOXIDE LEAK DETECTORS.
 ADD SECOND 14" D.I. WALL PIPE AS SHOWN IN BAR SCREEN MECHANICAL PLAN.



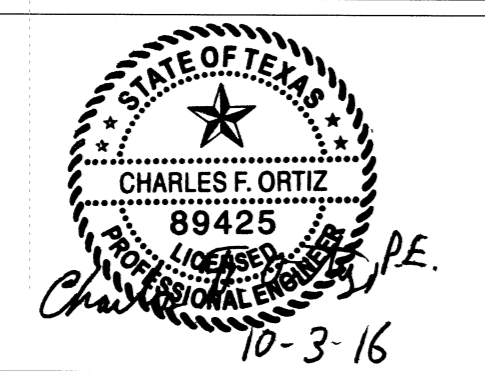
CHLORINATION AND DECHLORINATION MECHANICAL PLAN SCALE: NTS



BAR SCREEN MECHANICAL PLAN SCALE: NTS



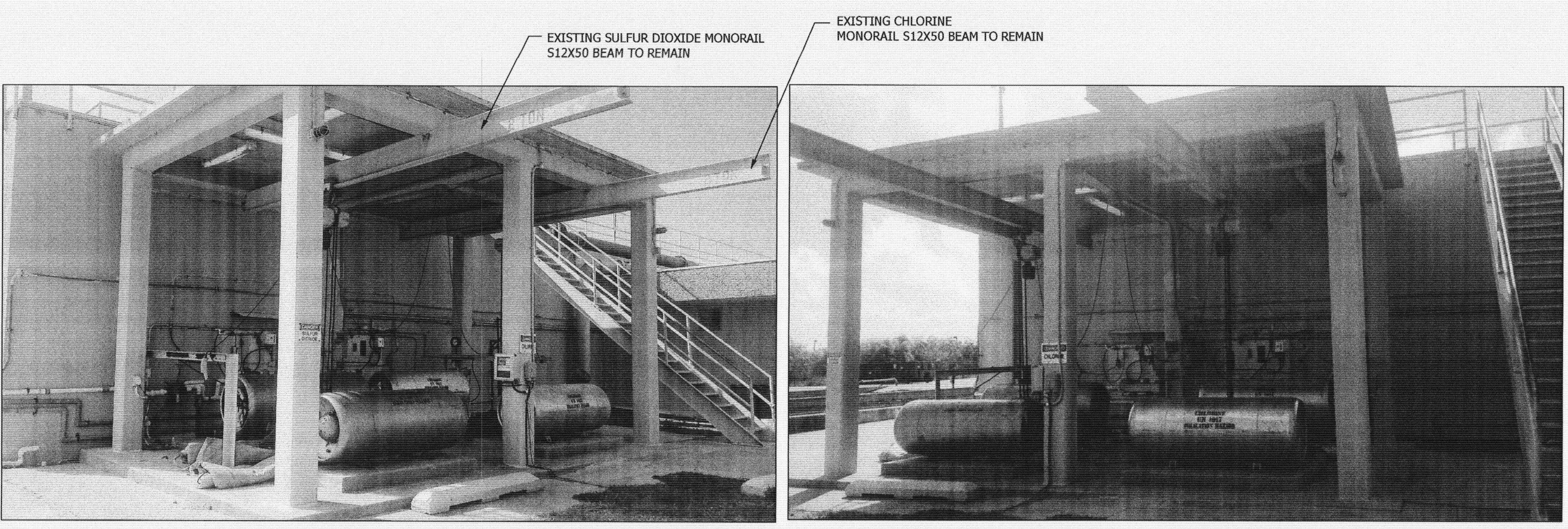
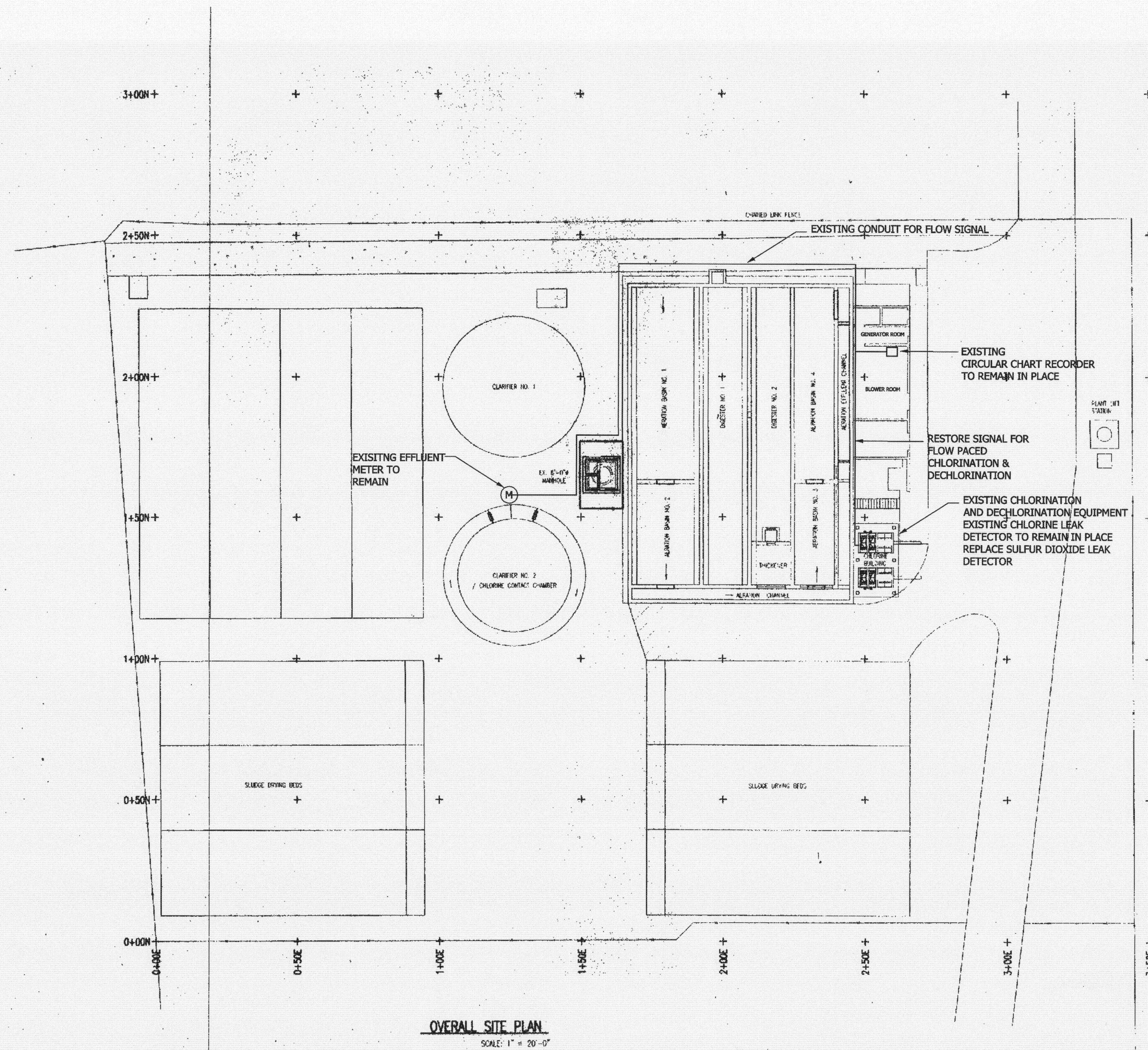
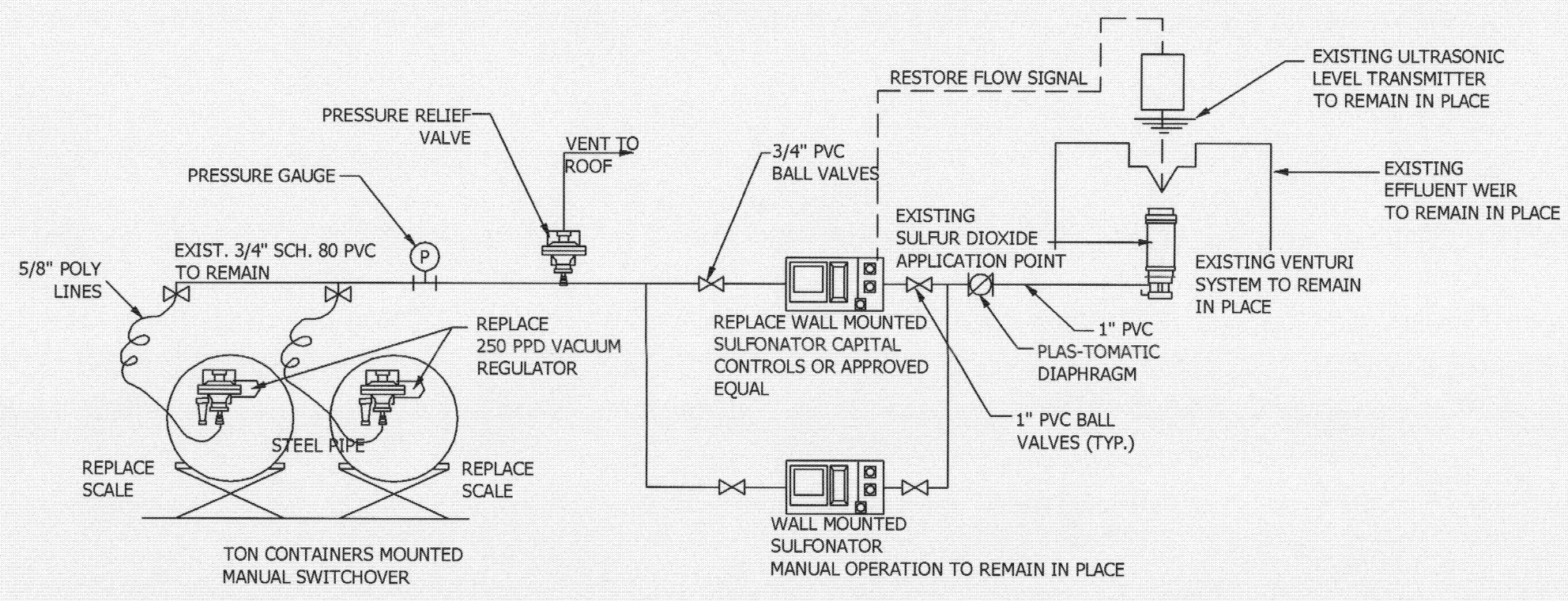
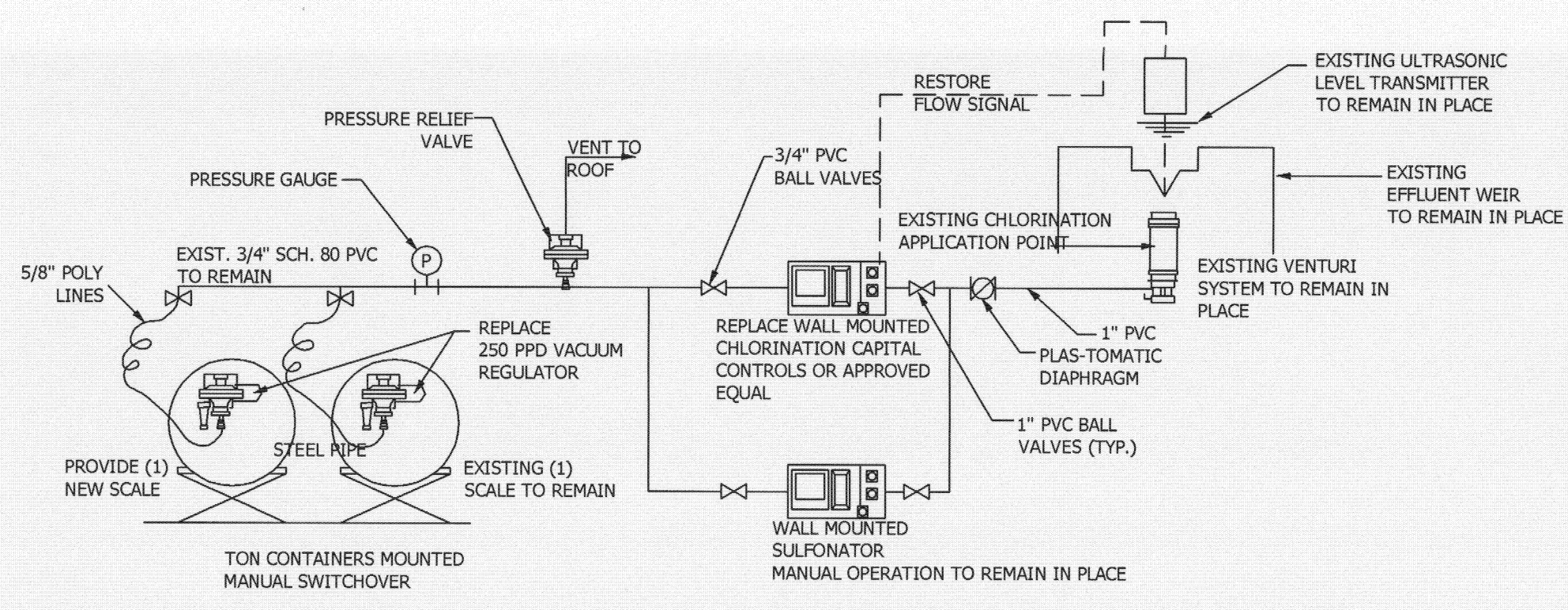
BAR SCREEN MECHANICAL SECTION (TYP. 2 PLACES) SCALE: NTS



Laguna Madre Water District
 Wastewater Treatment Plants Rehabilitation
 September 2016

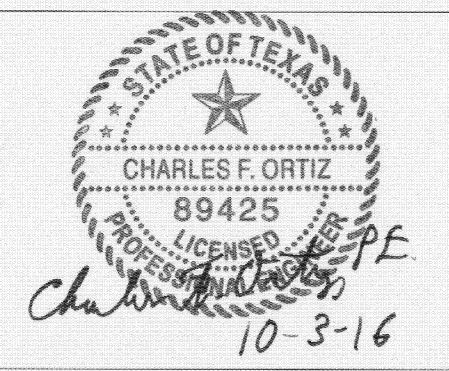
Laguna Madre Water District
 Andy Bowie Wastewater Plant
 Chlorination & Dechlorination Equipment





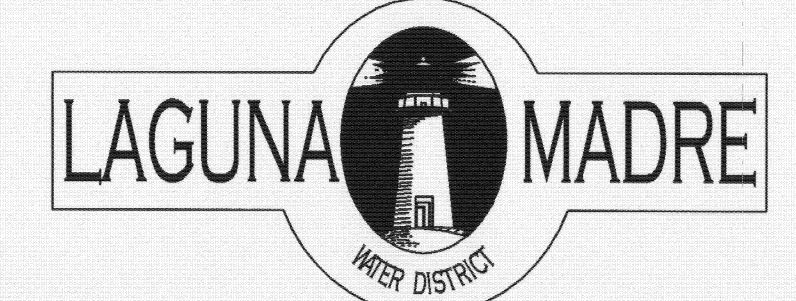
- CHLORINE HOIST NOTES**
1. MONORAIL (EXISTING S12X50 BEAM TO REMAIN)
 - A. REPLACE NUTS AND BOLTS TO COMPLY WITH ANSI-B30.11-1.3.1(b). USE BEVELED WASHERS
 - B. PROVIDE A NEW FESTOON SYSTEM FOR ELECTRIFICATION / POWER.
 2. REPLACE TROLLEY AND HOIST. SEE SECTION 467400-HOIST IN SPECIFICATIONS.
- SULFUR DIOXIDE HOIST NOTES**
1. MONORAIL (EXISTING S12X50 BEAM TO REMAIN)
 - A. REPLACE NUTS AND BOLTS TO COMPLY WITH ANSI-B30.11-1.3.2(b). USE BEVELED WASHERS.
 - B. PROVIDE A NEW FESTOON SYSTEM FOR ELECTRIFICATION/POWER.
 2. REPLACE TROLLEY AND HOIST. SEE SECTION 467400-HOIST IN SPECIFICATIONS.

NOTES:
 ADDENDUM No1: SIZE ALL PROPOSED ROTAMETERS FOR 250 PPD. DISTRICT DOES NOT USE INDUCTION PUMPS FOR CHLORINATION AND DECHLORINATION EQUIPMENT. EXISTING VENTURI SYSTEM TO REMAIN IN PLACE. AUTOMATIC SWITCHOVER REMOVED FROM ALL VACUUM REGULATORS. RESTORE EJECTORS AT ALL SITES.



Laguna Madre Water District
 Wastewater Treatment Plants Rehabilitation
 September 2016

Port Isabel WWTP
 Chlorination & Dechlorination
 Equipment



DESIGN DATA

INFLUENT PARAMETERS

WET WEATHER PARAMETERS

30 Day - Average Wet Weather Flow	(mgd)	0.65
Peaking Factor		3.00
Two-Hour Peak Flow	(mgd)	1.95
Average BOD5	(mg/L)	200.00
Average TSS	(mg/L)	200.00
Average BOD5 Loading	(lbs/day)	1084.20
Average TSS Loading	(lbs/day)	1084.20

EFFLUENT PARAMETERS

Maximum Average BOD5	(mg/L)	10.00
Maximum Average TSS	(mg/L)	15.00
Minimum Dissolved Oxygen	(mg/L)	4.00

AERATION BASIN DESIGN

AERATION BASIN

Length	(ft)	120.00
Width	(ft)	80.00
Side Water Depth	(ft)	9.00
Volume Available	(cu. ft.)	86400.00
	(gallons)	646,272
Existing Design Organic Loading	(lb BOD5/day/1000 cf)	12.55
State required Organic loading	(lb BOD5/day/1000 cf)	45.00

AERATION REQUIREMENTS

Design Organic Loading	(lbs/day)	1084.20
State Air Criteria	(lb O2 required/lb BOD5)	1.20
lb O2 required for BOD5	(lbs/day)	1301.04

STATE CRITERIA AIR REQMTS

	(lbs/day)	1301.04
State Coarse Bubble O2 Transfer Factor Req'mt		0.65
Clean Water Transfer Efficiency (Manufacturer)	#NAME?	10.00%
Wastewater transfer efficiency	(%)	6.50%
State Criteria for Air Requirements	(cu. ft/minute)	805.80
STATE CRITERIA AIR REQMTS	(cu. ft/minute)	805.80

CLARIFIER DESIGN

Two-Hour Peak Flow	(mgd)	1.95
Existing Number of Clarifiers		2.00
Existing Diameter for each Clarifier	(ft)	46.00
Existing Surface Area per Clarifier at Peak Flow	(sq. ft.)	1661.91
Existing Surface Loading at Peak Flow	(gpd/sq. ft.)	586.68
State req'd Max Surface loading at Peak Flow	(gpd/sq. ft.)	800.00
Existing Surface Loading at Design Flow	(gpd/sq. ft.)	195.56
State req'd Max Surface loading at Design Flow	(gpd/sq. ft.)	600.00
Existing Side Water Depth	(ft)	12.00
Total Existing Surface Area	(sq. ft.)	3323.81
Total Clarifier Volume	(cu. ft.)	39885.75
	(gallons)	298345.44
State required Detention Time at Peak Flow	(hours)	1.50
Actual Detention Time at Peak Flow	(hours)	3.67
State required Detention Time at Design Flow	(hours)	3.00
Actual Detention Time at Design Flow	(hours)	11.02

RETURN ACTIVATED SLUDGE UNDERFLOW RATE

Underflow Rate	(gpd/sq. ft. of clarifier)	400.00
RAS Flow for each Clarifier	(gpd)	132925.12
	(gpm)	923.28
Existing Maximum RAS Flow per Clarifier	(gpm)	780.00

AEROBIC DIGESTERS VOLUME

AEROBIC DIGESTER BASIN NO. 1		
Length of Basin	(ft)	44.00
Width of Basin	(ft)	22.00
Side Water Depth	(ft)	14.00
Volume of Basin	(cu. ft.)	13552.00
	(gallons)	101268.96
Total Digestion Volume Proposed	(cu. ft.)	13552.00
	(gallons)	101268.96

SLUDGE PRODUCTION

Influent BOD Loading	(lbs/day)	1084.20
Effluent BOD Loading	(lbs/day)	54.21
BOD Removed from Process (S)	(lbs/day)	1029.99
Design SRT (Theta)	(Days)	8.00
Design MLSS	(mg/L)	4200.00
Aeration Volume Available	(mg)	0.101
Gross Yield Coefficient (Y)	(mg VSS/mg BOD)	0.60
Decay Coefficient (Kd)	(day-1)	0.060
Biological Solids Production (lbs VSS/day)	[$P_x = Y * S_r / (1 + (K_d * \theta))$]	417.56
% Non-Volatile SS from Influent SS (INV)	(%)	45%
Non-Volatile SS into Process (INV)	(lbs/day)	487.89
Effluent SS (E)	(lbs/day)	81.52
Waste Activated Sludge Production (WAS)	(lbs/day)	824.14
Solids Yield (y)	(lbs TSS/lb BOD)	0.80
Total Solids Production	(lbs of TSS)	6593.11
Solids Allowed in Aeration Basin	(%)	3550.75
Percent of VSS in Sludge Produced	(%)	80.00%
Percent Destruction of VSS	(%)	38.00%
Sludge Produced for Dewatering	(lbs/day)	373.60
Solids % Concentration in Digesters	(%)	2.00%
Sludge Retention Time in Digesters	(Days)	29

AEROBIC DIGESTERS AIR REQUIREMENTS

State Criteria air requirements for Digesters	(scfm/1000 cu. ft.)	30.00
State Criteria air required for Digesters	(scfm)	406.56

CHLORINATION CONTACT TIME REQUIREMENTS

Peak Flow Through Chamber	(mgd)	1.95
Existing No. of Chambers		2.00
Existing Length of Each Chamber	(ft)	22.00
Existing Width of Each Chamber	(ft)	11.00
Existing Surface Water Depth	(ft)	10.00
Existing Total Chlorine Contact Volume	(gallons)	4840.00
		36203.20

State required Contact Time at Peak Flow	(minutes)	20
Existing Contact Time at Peak Flow	(minutes)	27
Existing Volume for Chlorination	(gallons)	36203.20
	(cu. ft.)	4840.00

CHLORINATION AIR REQUIREMENTS

DO level required before discharge	(mg/L)	4.00
lbs of O2 required in Chlorination chamber (AOR)	(lbs/day)	65.05
State Coarse Bubble O2 Transfer Factor Req'mt		0.65
Clean Water Transfer Efficiency	#NAME?	10.00%
Wastewater transfer efficiency	(%)	6.50%
AIR REQUIREMENTS FOR CHLORINATION	(cu. ft/minute)	40.29

CHLORINATOR CAPACITY REQUIREMENTS

Peak Flow	mgd	1.95
Chlorine Dosage	mg/L	10.00
Chlorinator Capacity Required at Peak Flow	lbs/day	162.63
Existing Number of Chlorinator Feeders		2.00
Capacity for each Chlorine Feeder	lbs/day	500.00

AIR LIFT PUMPS AIR REQUIREMENTS

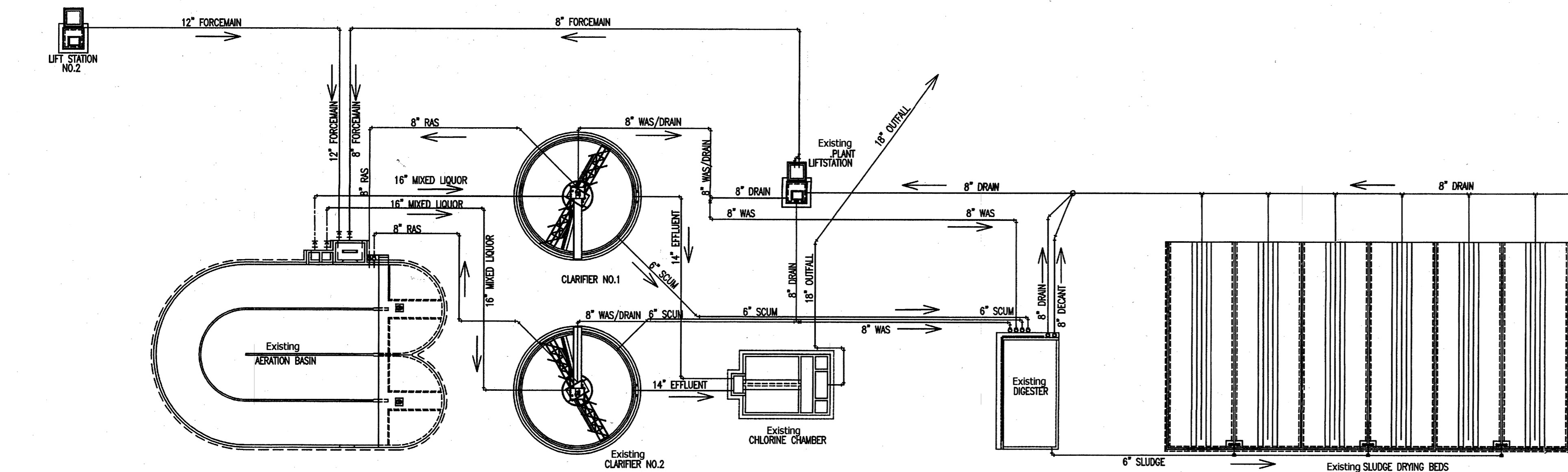
Number of 6" airlift pumps		2.00
Number of 10" airlift pumps		1.00
Air requirements per 6" airlift pump	(scfm)	25.00
Air requirements per 10" airlift pump	(scfm)	100.00
Air requirements for all 6" airlift pumps	(scfm)	50.00
Air requirements for all 10" airlift pumps	(scfm)	100.00
Total air requirements for airlift pumps	(scfm)	150.00

TOTAL AIR REQUIREMENTS

AERATION REQUIREMENTS	(SCFM)	805.80
DIGESTION REQUIREMENTS	(SCFM)	406.56
CHLORINATION REQUIREMENTS	(SCFM)	40.29
AIR LIFT PUMPS REQUIREMENTS	(SCFM)	150.00
TOTAL AIR REQUIREMENTS	(SCFM)	1402.65

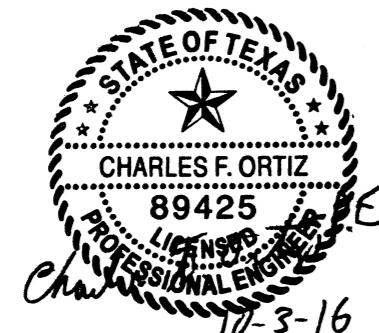
NOTE: AIR IS SUPPLIED BY TWO (2) BLOWERS RATED EACH AT A DESIGN FLOW OF 844 CFM AT 6.8 PSIG WITH 40 H.P. MOTORS. ONE (1) BLOWER WILL REMAIN IN PLACE. PROPOSED ONE (1) BLOWER AT A DESIGN FLOW OF 600 CFM AT 6.8 PSIG WITH 30 H.P. MOTOR.

NOTES
ADDENDUM No. 1: CHANGED "PROPOSED" TO "EXISTING" AS NEEDED TO SHOW EXISTING CONDITIONS. REVISED PROPOSED HIGH SPEED TURBO BLOWER, MODEL No. TO NX30-C050 OR APPROVED EQUAL.



PROCESS FLOW SCHEMATIC

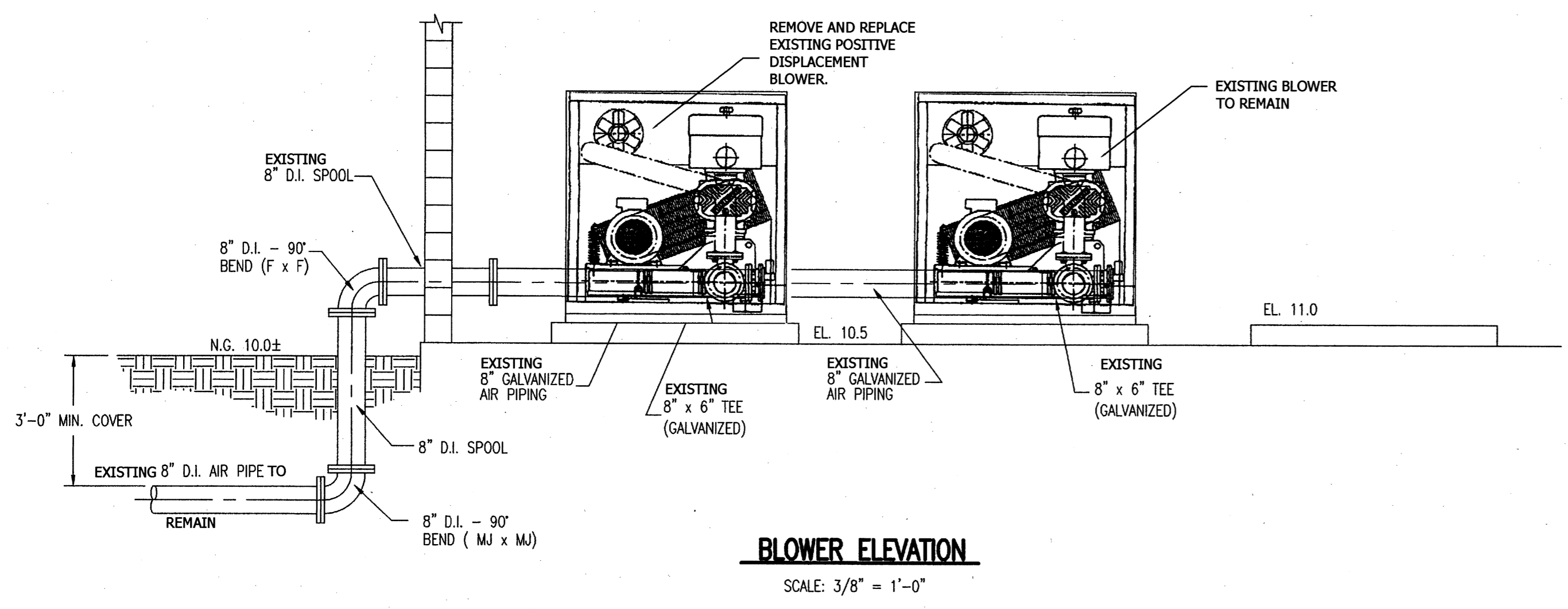
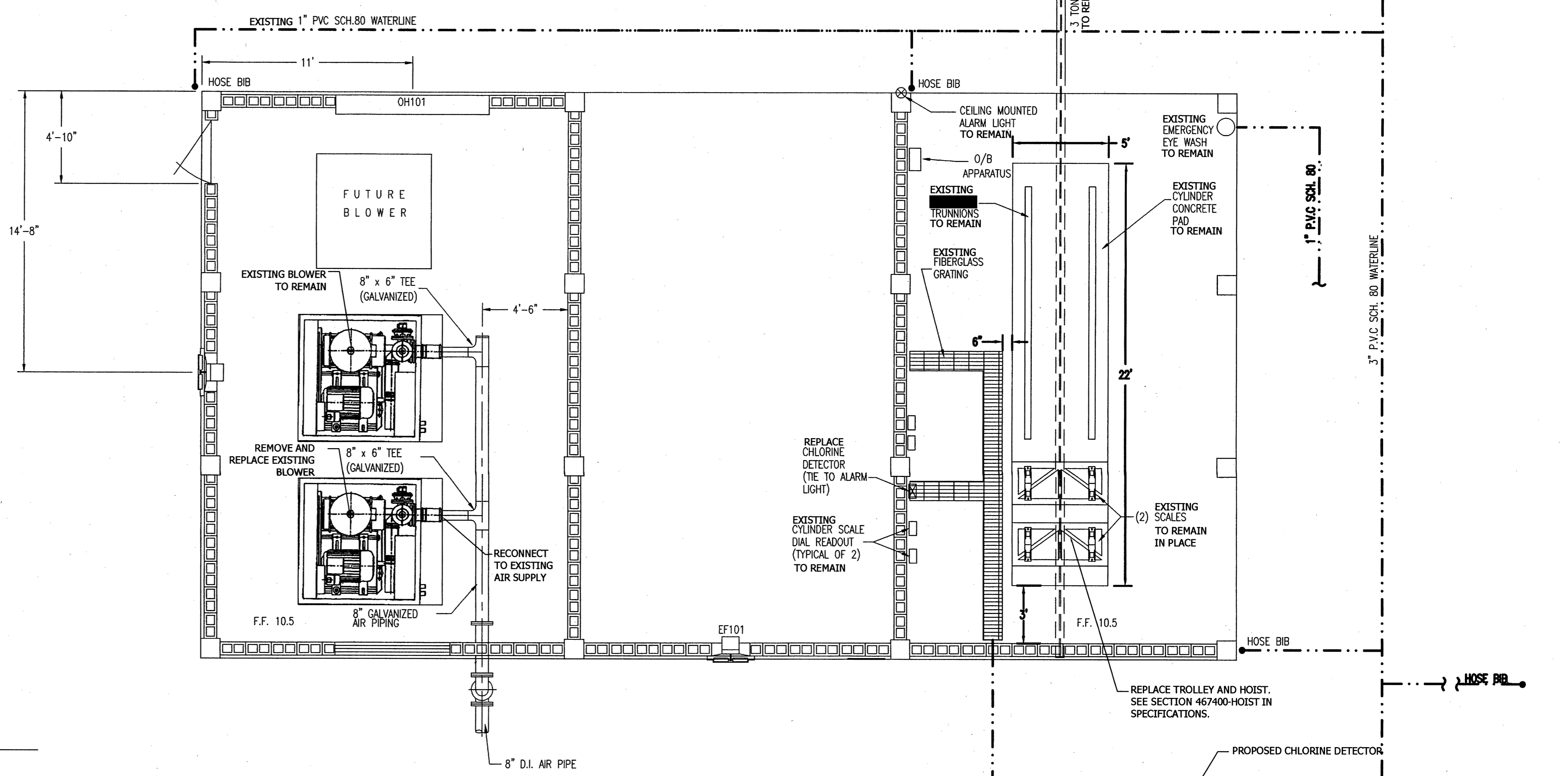
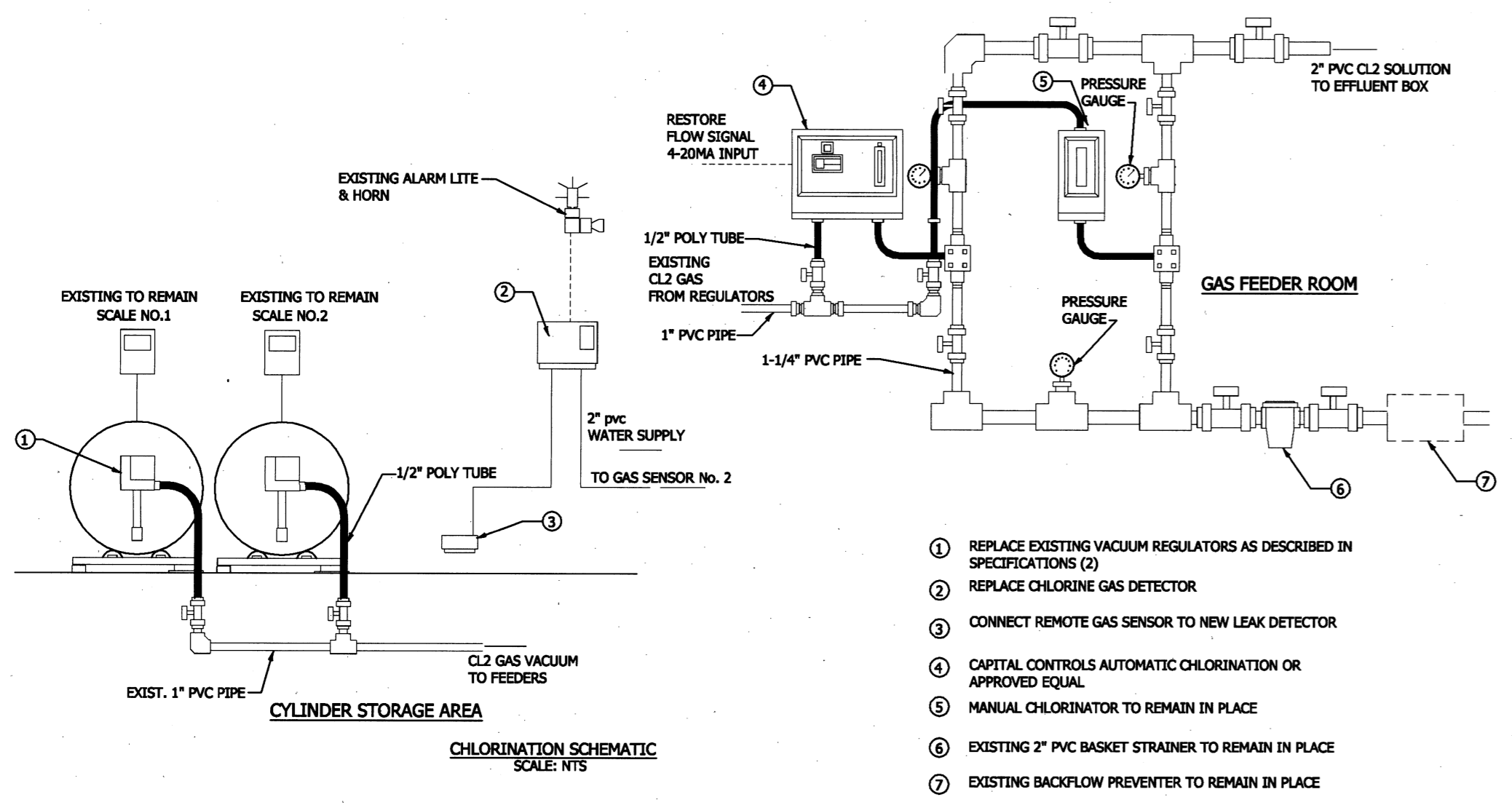
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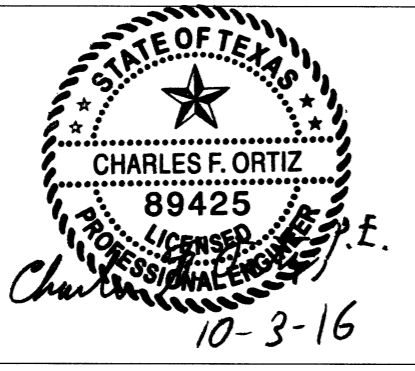
Laguna Madre Water District
Wastewater Treatment Plants Rehabilitation
September 2016

Laguna Vista WWTP
Design Data And Process Schematic





NOTES
ADDENDUM No.1: REVISED PROPOSED HIGH SPEED TURBO BLOWER, MODEL No. TO NX30-C050 OR APPROVED EQUAL PROVIDE DUAL SENSOR FOR CHLORINE LEAK DETECTOR.



Laguna Madre Water District
Wastewater Treatment Plants Rehabilitation
September 2016

Laguna Vista WWTP
Chlorine System Feed/Blower
Building Mechanical Modifications

